Planar ZEBRA Battery for Renewable Integration and Grid Applications

Beyond Lithium Ion, PNNL Richland WA June 7th- 9th 2011



Acknowledgements

- □ ARPA-E Storage Program
 PNNL directed R&D fund
- ☐ Staff at PNNL:

Battery Team: Xiaochuan Lu, Guosheng Li, Vincent Sprenkle, Brent Kirby, Nathan Canfield, Jeff Bonnett, Richard Pearson, Eric Mast, Gary Yang, Kerry Meinhardt.

NMR Team: Jianzhi Hu, Mary Wu, Ju Feng

Project support: Jud Virden, Jun Lui, Gordon Graff

□ EaglePicher: Bob Higgins, Jim Degruson, Dave Lucero



Na-beta alumina membrane batteries (SBB)

SBB are electrochemical devices that store electrical energy via Na⁺ transport through conductive solid oxide membrane (typically β "-Al₂O₃) at elevated temperatures.

➤ Sodium-sulfur (SSB)

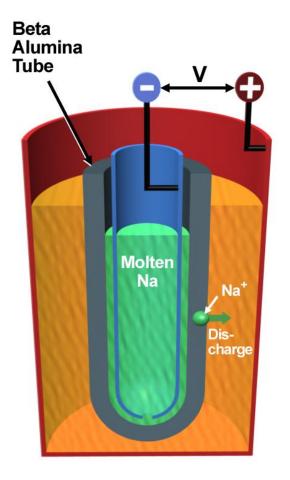
$$2Na + 4S \stackrel{C}{\longleftrightarrow} Na_2S_4 E=~2.0 V$$

Sodium-metal chloride (ZEBRA)

$$2NaCl + Ni \stackrel{C}{\longleftrightarrow} NiCl_2 + 2Na E=~2.58 V$$

- Operated at 300~350°C
- □ High efficiency, up to >90%
- Capable of hours of discharge duration
- Quick response
- Up to 16MWhs demonstrated, for SSB

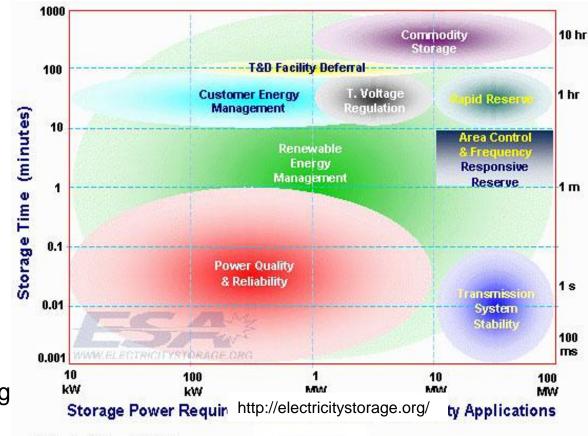
Invented and first investigated by Ford for vehicle applications





Technology requirements for GRID Storage

- Energy/power: depending on applications;
- Quick response preferable;
- Discharge duration: seconds ~ hours
- Efficiency: High, preferable;
- Life: >10~15yrs, >5,000 deep cycles, higher for shallow cycles, depending on applications;
- Safety



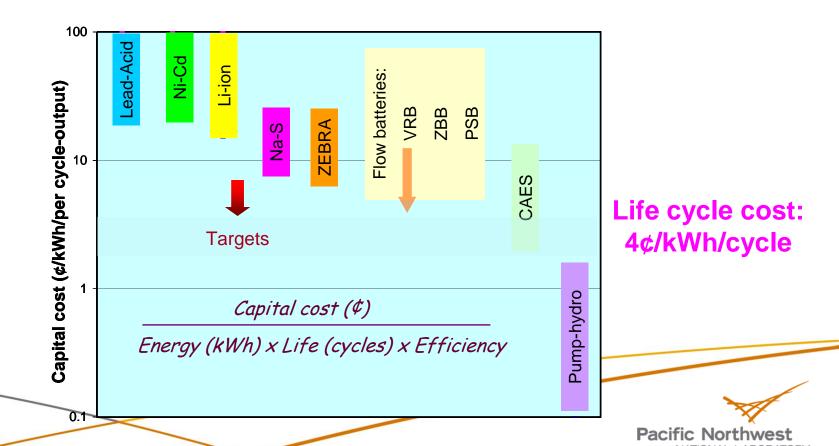
Data from Sandia Report 2002-1314

Costs: low capital cost, life cycle cost, social cost (considering carbon effects)



Economic and technical challenges

- Cost at least 2~3 x higher for broad market penetration
- Better economy reliant on improved reliability, durability, life and efficiency, along with manufacturing
- Require science and technology advancement

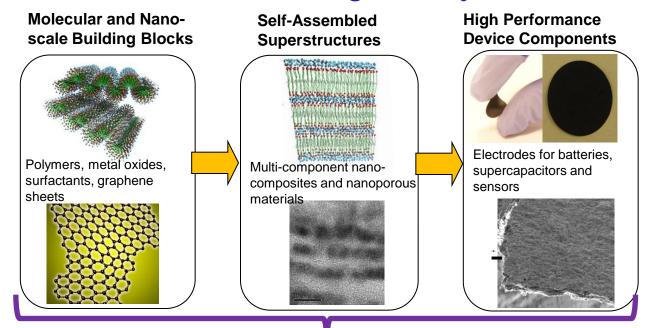


Electrochemical Energy Storage at PNNL

Transformational Materials Design and Synthesis

Key Focus:

- Synthesis and assembly of multifunctional nanomaterials
- Establish controlled defect chemistry and architectures
- Optimization of properties that effect transport and storage of charged species.



High Power Planar Sodium Metal Halide

High Performance Lithium Ion

Redox Flow Batteries V based and PV Charging

Electrolyte

Catholyte

Large area planar call -> hattery stack



REVIEW pubs.acs.org/CR

Electrochemical Energy Storage for Green Grid

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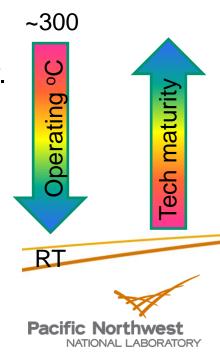
I₁O₂-base co rane

Olivine LiFePO₄

Na-Battery Focus Areas at PNNL

Progression of sodium battery technology

- Gen 1: High Temperature (250-300°C), BASE
 - Modular planar design (flat plate), tunable power and energy.
 - Multi-metal cathode, decrease Ni.
 - Need for better fundamental understanding additives, mass transport.
- •Gen 2: Reduced Temperature (110-250°C),
 - Approach to low cost and higher power density.
 - Na ion conducting membrane.
 - Stable catholyte
- •Gen 3: Low Temperature (RT- 90°C),
 - Approach to Na-ion (polymer membrane)
 - Anode materials
 - High energy capacity cathode.



Sodium Ion Research Opportunities

	Generation 1 High Temp Planar 250 – 300C	Generation 2 Medium Temp Planar 110-250C	Generation 3 Low Temp RT – 90C
Application	Stationary	Stationary Light Truck Marine DOD	VT
Chemistry	 Na-NiCl₂ Na-NiFeCl₂ 	Na-Metal HalideNa-Na organicNa-Air	Na-SNa-Metal oxideNa-Air
Anode	Molten NaBASE wetting agents.	Molten NaBASE wetting agents.	Na MetalNa AlloyNa-MSNaCxFNaMxOy (Ti, Sn)
Cathode	Ni-NiCl2(s)/NaAlCl4Ni Alloys-NiMClxAdditives	Mx-MxCl2(sol), IL, CxOrganic-Na organic	NaMxOy (Ni,Mn, Co)NaMPO4NaMxFyNa-organic
Electrolyte	• BASE	BASENew SS inorganicOrg-InorgNanocomposite	Polymer Membrane-Liq SS inorganic glass

Down-select areas of high value with preliminary performance and cost modeling. Further down-select chance of success using thermodynamic and phase diagram based analysis.

Medium Temperature Na-MH Concepts

- Goal: Reduce temperature (100-250°C enables lower materials cost, (sealing, cell materials).
- Path: 1) Reduce BASE thickness, 2) Improve catholyte

ZEBRA type chemistry: insoluble MH

Ni + 2NaCl
$$\rightarrow$$
 2Na + NiCl₂ (charge)
NiCl₂+2Na \rightarrow 2NaCl + Ni (discharge)







NiCl₂ (insoluble)

Metal coated chemistry: soluble MH

 $EC/M_x + NaCl \rightarrow Na + M_xCl_y + EC$ (c) $EC + M_xCl_y + Na \rightarrow NaCl + EC/Mx$ (d)

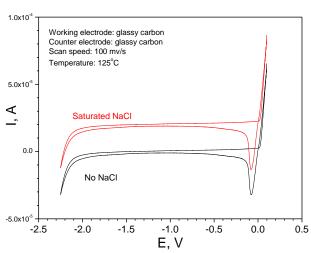


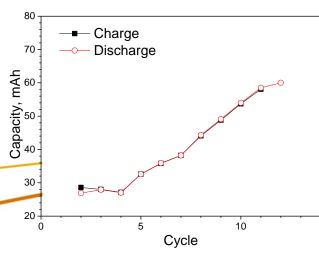




M_x Coated

 M_xCI_y (soluble)



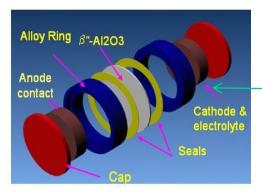


Medium Temperature Na- Air with BASE

Goal: Improve performance, low cost alkali metal – air.

Path: Improve solubility of Na_xO_y products in cathode with higher temperature.

3.0cm² Button Cell



Replace metal cathode with temperature stable air cathode.

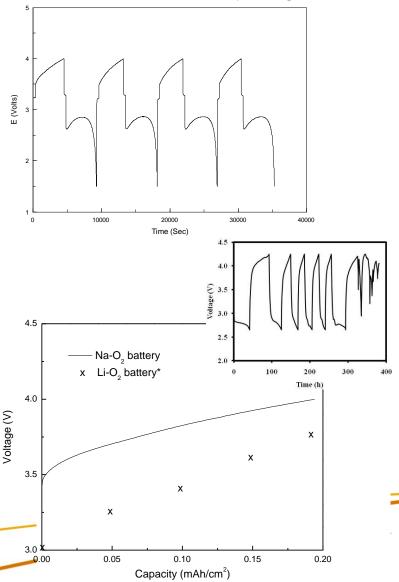
Cell Characteristics:

Temperature: 140°C OCV: 3.2V vs Na Current: 0.15mA/cm².

Summary:

- High IR from BASE electrolyte.
- Cycled in air, capacity decreases.
- Overpotential on charge higher than Li.
- Overpotential increase rate lower than Li.

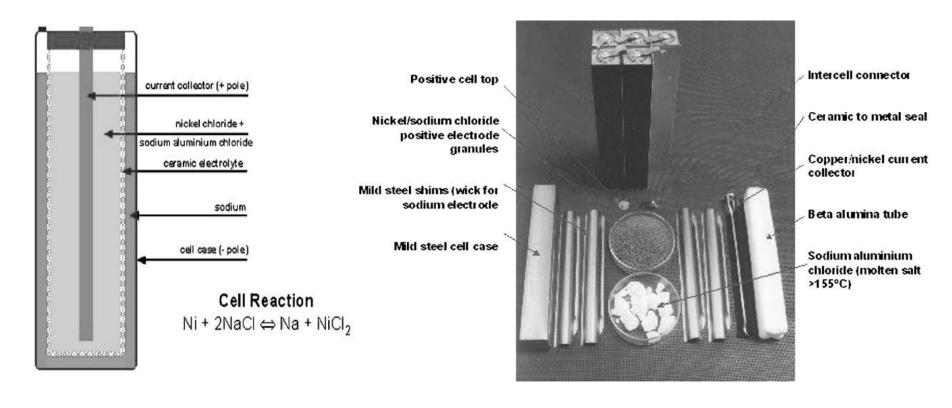
Na-Air Low rate cycling



^{*} J. Xiao, et al., J. Power Sources 196 (2011) 5674.

Na-Metal Halide - ZEBRA Battery

Beta Research and Development Ltd.



Advantages: High energy density, cycle life, short circuit failure mode, low cost materials, manufactured in discharged state.

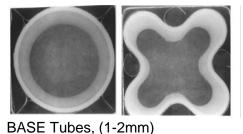
Disadvantages: High IR, molten Na, high operating temperature.



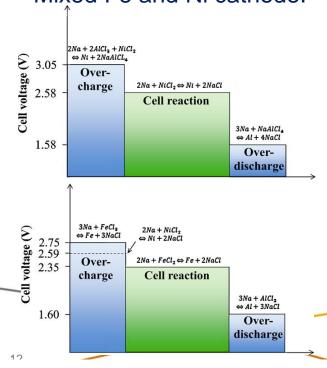
Na-Metal Halide - ZEBRA Battery

Beta Research and Development Ltd. high power cells.

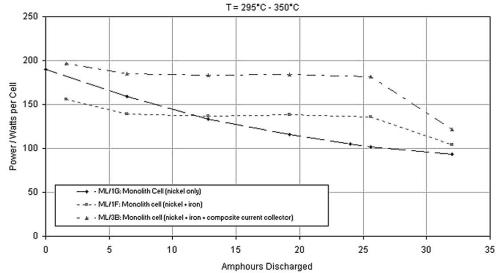
Decrease geometric factor.



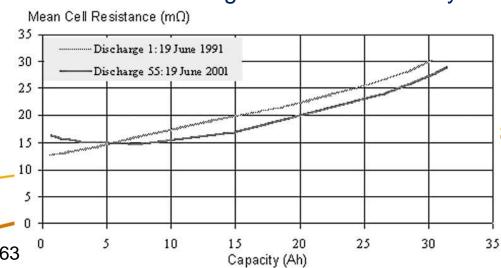
Mixed Fe and Ni cathode.



Pulsed power characteristics vs DoD

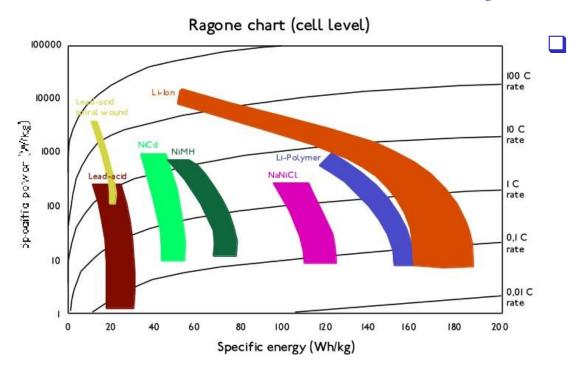


Effects of self discharge and freeze thaw cycles.



Sudworth, J. L. *J. Power Sources*, **100**, 2001, 149-163

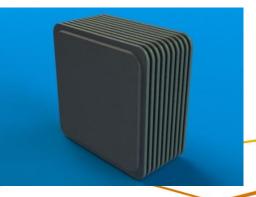
Na-metal halide battery development



MESDEA and FZ Sonick (joint venture b/w FIAMM MESDEA) for both mobile and stationary applications



Eagle Picher developing planar designs

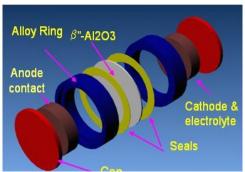


General electric for locomotive and backup power applications



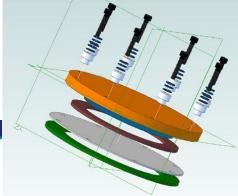
Path to Planar Na Battery

3.0cm² Button Cell



Materials development and performance testing.

64cm² XL-Button Cell



Materials scale-up with large-scale performance and life testing.

Ceramic Window Frame Contact material Electrolyte

100cm² Planar Cell

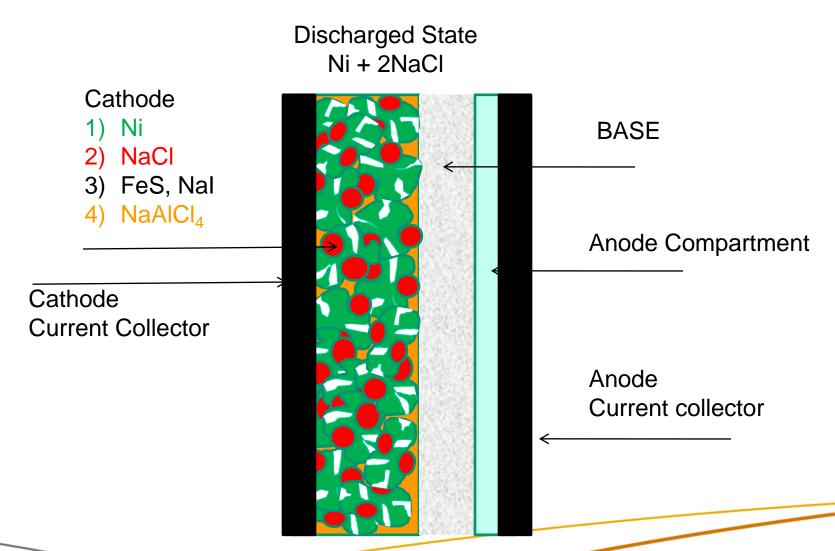
Manufacturing friendly components and fabrication techniques.

200cm² Stack



Modular stack design with performance and life testing.

Na-NiCl₂ Battery Description





BASE Conversion Process

Mixed region of β and β " Na₂O·nAl₂O₃ (5.33 \leq n \leq 8.5).

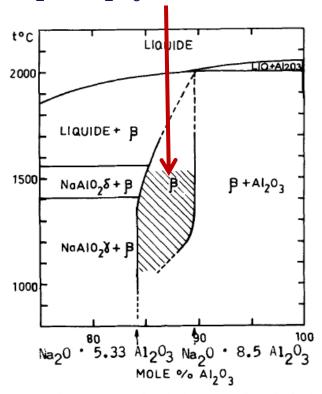
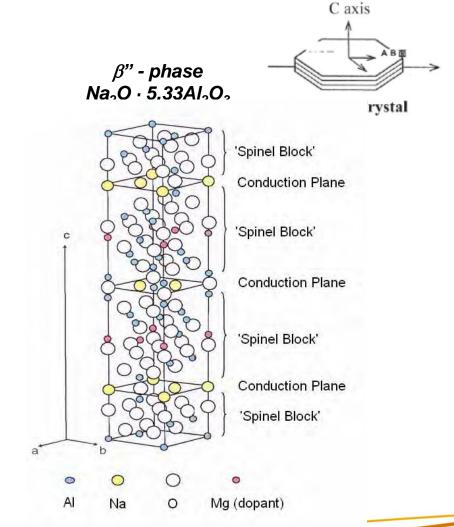


Fig. 1. Existence range of β -alumina. $\beta+\beta''$ coexist in the cross hatched region of the diagram.

Fally, et al JECS 120[10] 1973



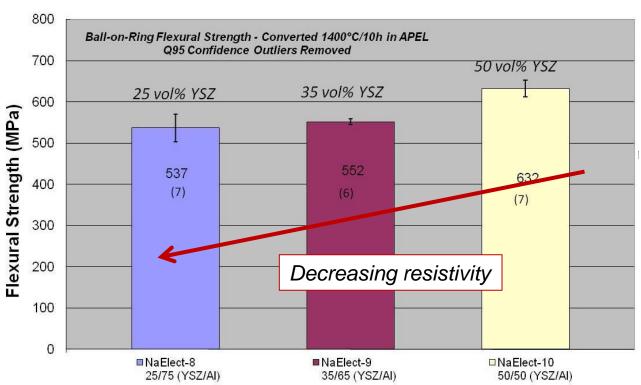
Journal of Ceramic Processing Research. Vol. 11, No. 1, pp. 86~91 (2010)

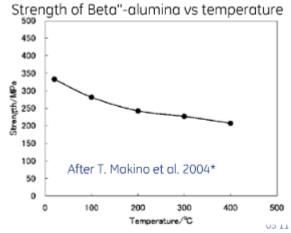
16

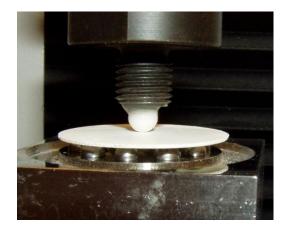
Complete conversion of Al₂0₃ to BASE is critical to consistent performance. Other factors influencing performance include, grain size, orientation, and density to avoid failure modes.

BASE Strength Properties

Flexural Strength (Mpa) vs Volume % YSZ in BASE





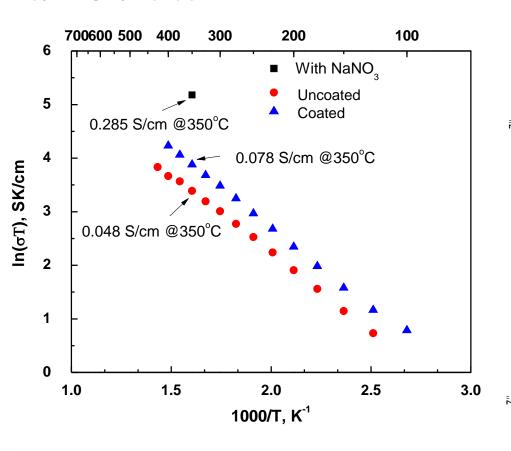


Optimize BASE formulation for strength and conductivity.

Ball on Ring flexural testing on 1.0" diameter converted BASE. 25 to 50% YSZ content.

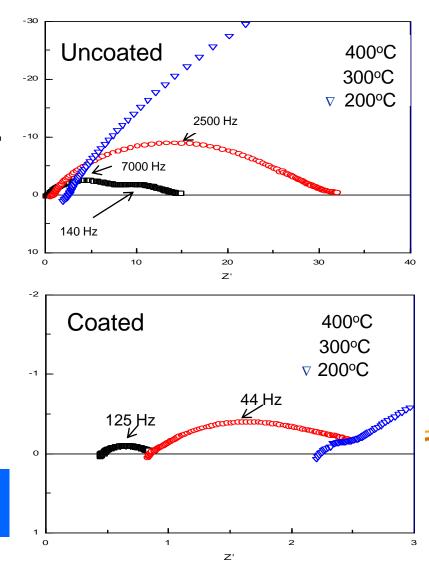
BASE Surface Properties(1mm)

Effect of BASE coating on β "-Al₂O₃ (Ionotec) conductivity at 200mA/cm² in Na/BASE/Na cell.



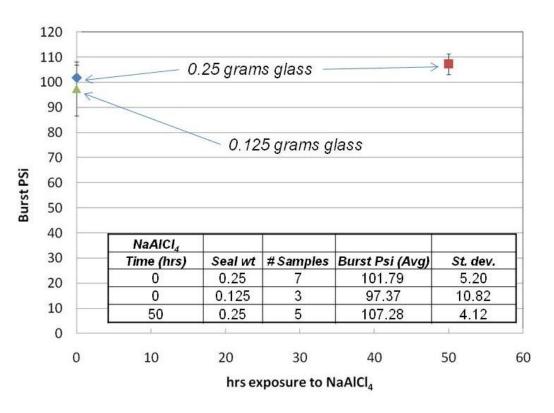
Large decrease in interfacial resistance as a function of surface and coating agents.

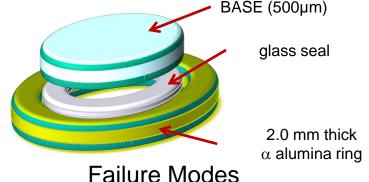
Comparison of interfacial resistance using EIS of Ionotec BASE in Na/BASE/Na Cell

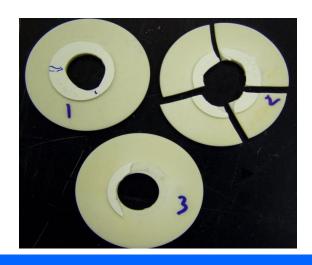


BASE/Seal Differential Pressure Test and Chemical Stability

Schematic of pressure sample assembly







Differential pressure in cell can reach 2 atm on cycling. Current seal holds 6atm DP, with only one failure at the seal. Larger cells use current collector as support structure.

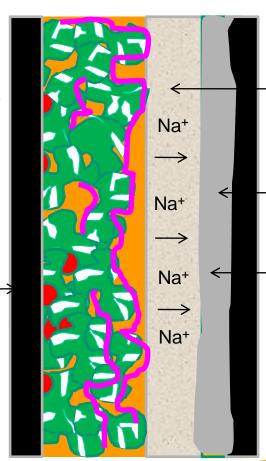
Na-NiCl₂ Battery Description

Charged State NiCl₂ → Na

Cathode

- 1) Ni
- 2) NaCl
- 3) FeS, NaI, NaF
- 4) NaAlCl₄
- 5) NiCl₂

Cathode
Current Collector



BASE

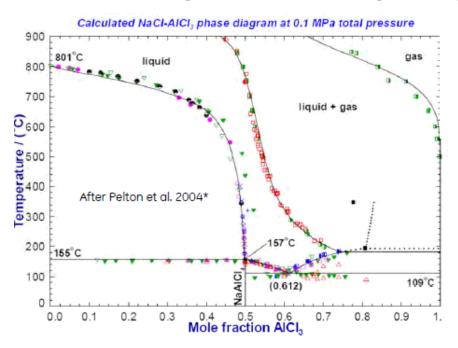
Anode Compartment

Na

- R increase as SOC as NiCl₂ deposits.
- Accessing NaCl deep in the cell becomes more difficult.
- Avoid over charging, melt turns acidic and NiCl₂ will dissolve.



Secondary Electrolyte (NaAlCl₄) Properties

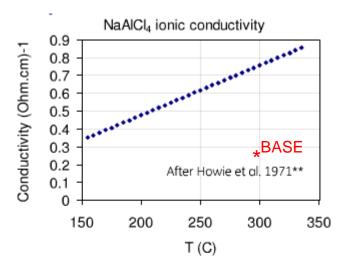


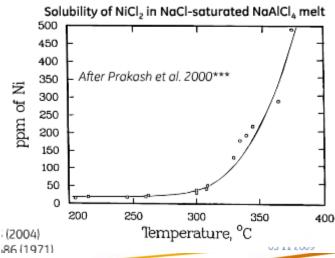
Basic

• (NiCl₄²⁻) formation. Solubility increases w/ temperature swings > 320°C, renders Ni electrochemically inaccessible.

Acidic

- Ni²⁺ increased solubility
- Localized acidic areas during high pulse power, Ni²⁺ detrimental to BASE





Non equilibrium conditions in melt affects performance and cycle life.

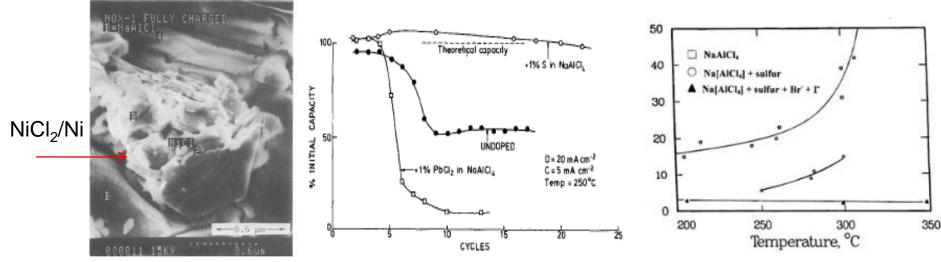
^{(*} C. Robelin et al. J. Chem. Therm. 36, 683 (2004)

^{**} Howie et al J. Inorg. Nucl. Chem., 33, 3686 (1971)

^{***} J.Prakash et al., J. Electrochem. Soc., 147502 (2000)

Cathode and SE (NaAICI₄) Sulfur Additives

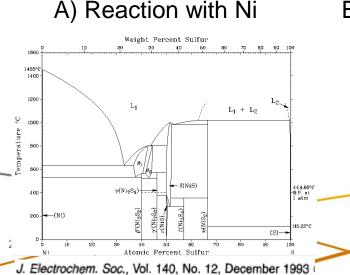
Role of S additives in charged state:



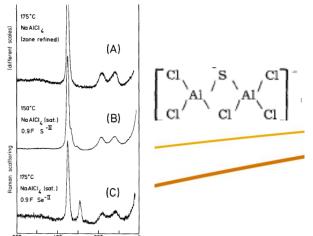
J. Electrochem. Soc., Vol. 136, No. 5, May 1989

Effect of S additive on cell capacity and NiCl₂ solubility in basic SE

Sulfur distribution in cathode:



B) Complex formation



C) Electrochemical

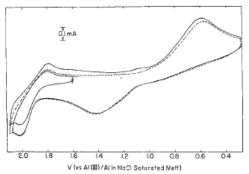
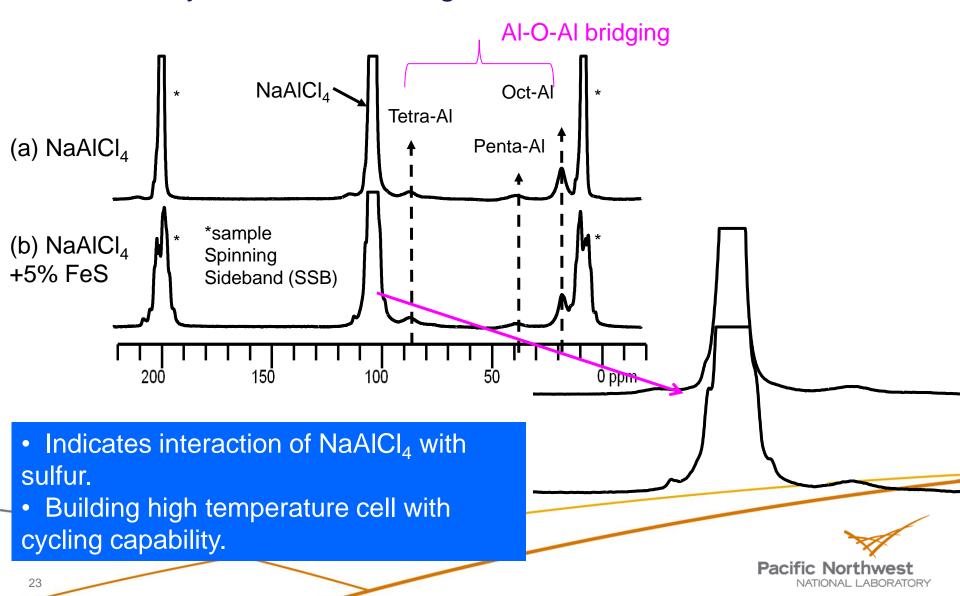


Fig. 2. Cyclic voltammogram at a glassy carbon electrode (area 0.07 cm²) in a 1.8 × 10-2 molal sulfur solution in NaCl-saturated melt at 175°C. Scan rate 0.1 V-sec⁻¹. Potentials vs. Al(III)/Al reference electrode in NaCl-saturated melt.

Cathode and SE (NaAlCl₄) Sulfur Additives

Preliminary Results: Ultra-high field ²⁷Al MAS NMR at PNNL

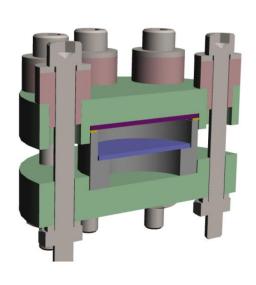


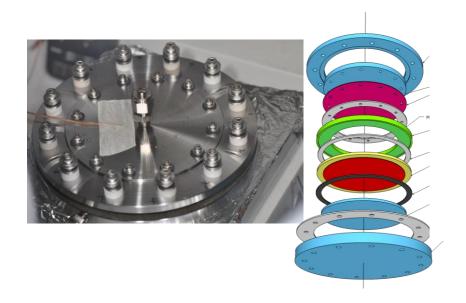
Cell Work Flow and Testing

Granule formulation → Ni, NaCl, Additives → Infiltrate

3cm² Research Cell (16 test stands)

64cm² Scale-up Cell 4 Test stands





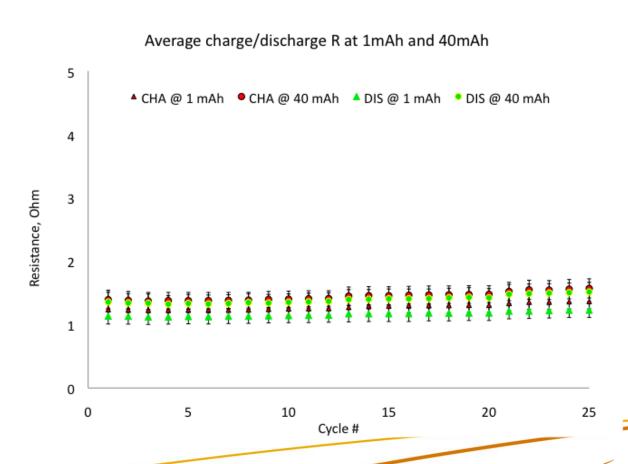
High power charging remains challenging due to small voltage window and increased resistance as function of SOC.



Na-Ni/NiCl₂ 3cm² Cell Reproducibility

150 Whr at 1C at 280°C

- Calculated from 3 replicate cells.
- Minimum resistance is 1
 Ohm due to BASE only.
- Maximum resistance before 3.0V cutoff is 4.5 Ohm.

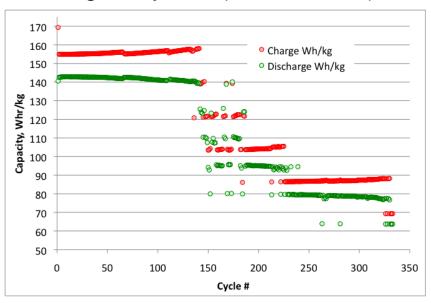




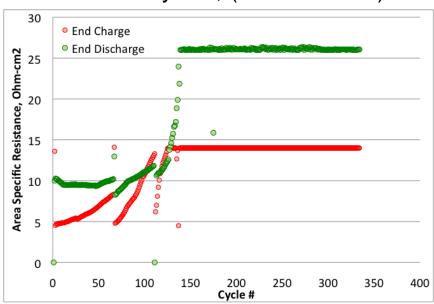
Na-Ni/NiCl₂ 3cm² Cell Performance

Cycle Conditions: 150Whr/kg (active cathode material) at 1C rate at 280°C

Whr/kg vs Cycles, (170mAhr cell)



ASR vs Cycles, (170mAhr cell)



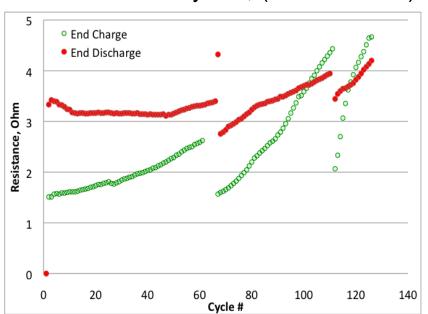
Resistance rise at end of charge dominates overall resistance rise.

- End of charge → NiCl₂
- Rising resistance →Loss of electron percolation path.
- End of discharge resistance increases later cycles.

Na-Ni/NiCl₂ 3cm² Cell Tear Down

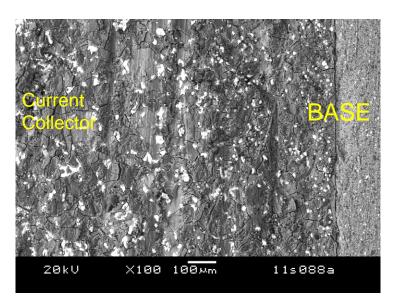
Cycle Conditions: 150Whr/kg (active cathode material) at 1C rate at 280°C

Resistance vs Cycles, (170mAhr cell)

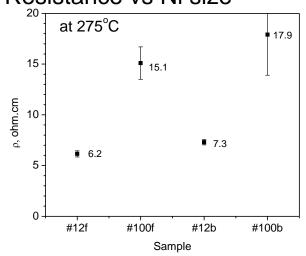


Probable cause for R increase

- Poor distribution of S additive.
- Decreased Ni granule size.
- Ni migration from BASE

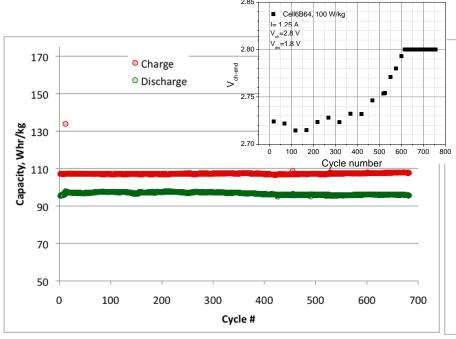


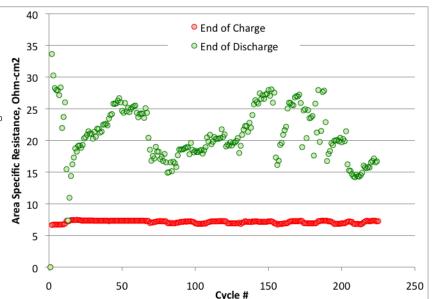
Resistance vs Ni size



Na-Ni/NiCl₂ 64cm² Cell Performance

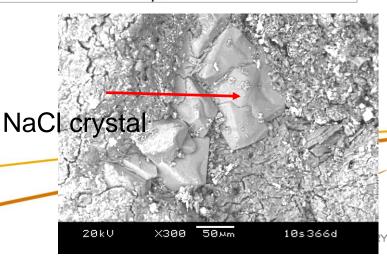
Cycle Conditions: 100Whr/kg (active cathode material) at 1C rate at 280°C





Performance analysis:

- For charging, larger amount of material, distribution of S additive.
- Decreased current density.
- NaCl grain grow effects discharge R.



Summary

- Planar configuration offers versatile power and energy cell design.
- ZrO₂ doped BASE lowers conversion temperature, improves strength.
- Reproducible BASE conductivity, however decrease by 3x compared to undoped BASE.
- Class seal pressure tested to withstand differential pressure of up to 6 atm. Robust chemical resistance to NaAlCl₄
- Developed new anode side BASE coating with improved wetting.
- Over 100 cycles at 150Wh/kg at 1C rate, for baseline chemistry in 3cm² cells. Developing new chemistry and additive approach to increase cycle life.
- Over 600 cycles at 100Wh/kg at 1C rate at 280C° for 64cm² cells.
- ▶ Developing 200cm² cell, with 20-30Ahr capacity.
- Developing integrated triple cell mini-stack.

