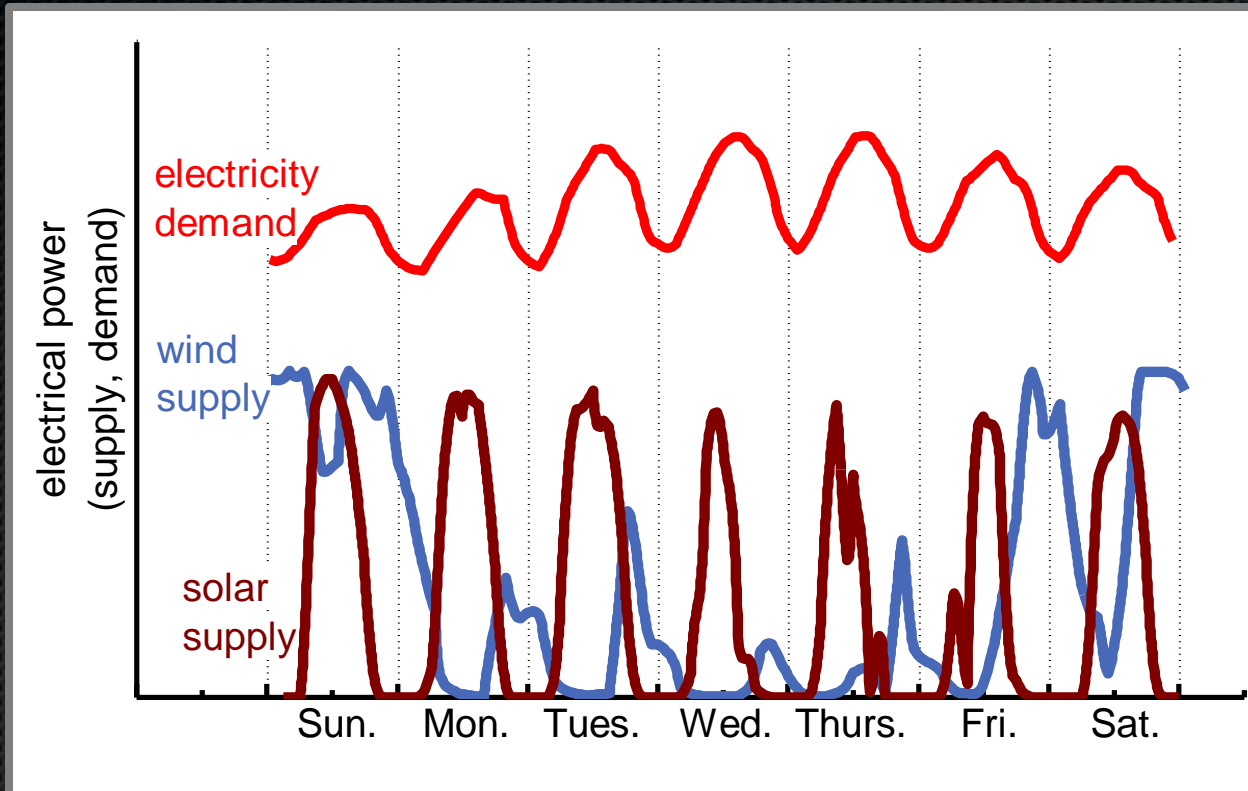




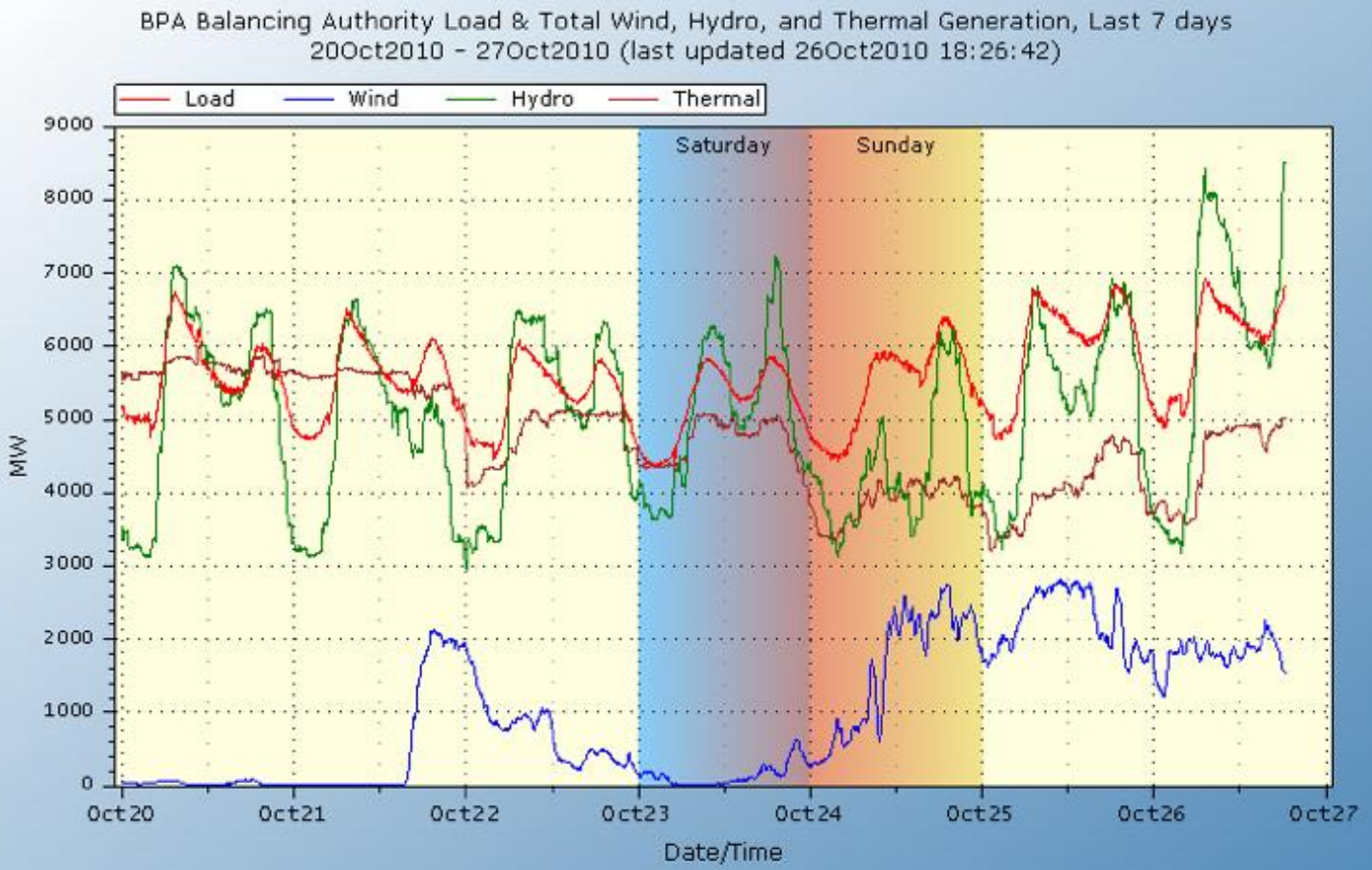
# An Electrometallurgical Approach to Cheap, Grid-Scale Energy Storage Systems

Luis A. Ortiz

# motivation



**storage is a key enabler for  
wind and solar renewable energy sources**



Based on 5-min readings from the BPA SCADA system for points 45583, 79687, 79682, and 79685  
Balancing Authority Load in Red, Wind Gen. in Blue, Hydro Gen. in Green, and Thermal Gen. in Brown  
Installed Wind Capacity=3011 MW  
BPA Technical Operations (TOT-OpInfo@bpa.gov)

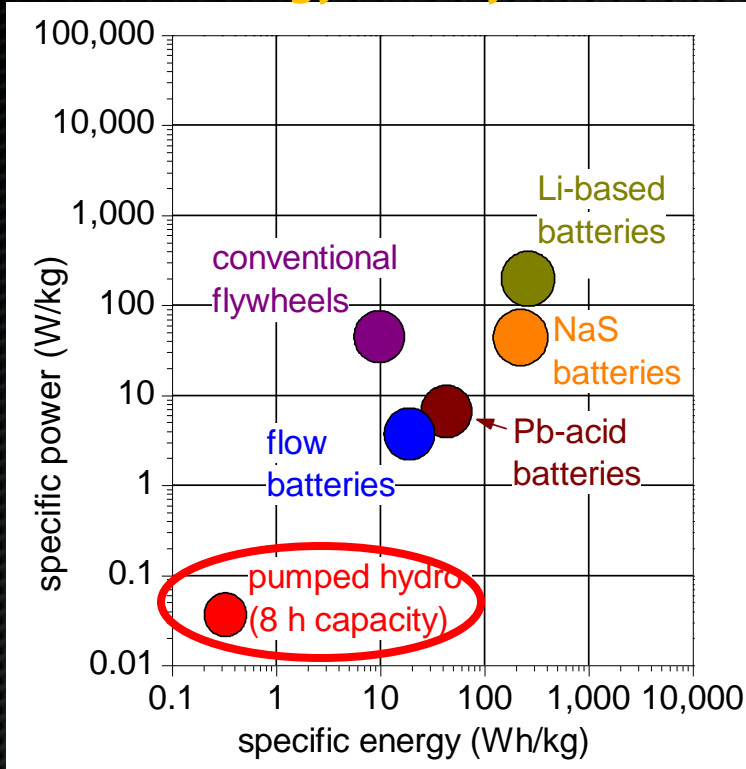


# cost as a driver of innovation

- ◉ grid-scale applications very attractive
- ◉ installed capital cost is a premium
  - ☞ best technical alternative is fossil fuel generation
- ◉ different requirements than portable energy storage

# key requirements

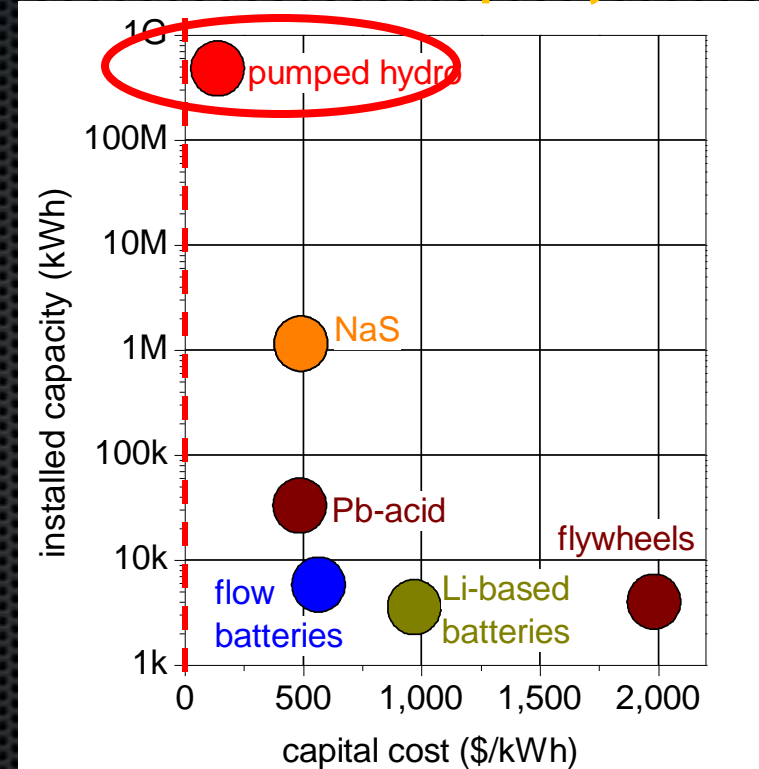
## energy density



### conventional metrics:

1. power density
2. energy density

## installed capacity

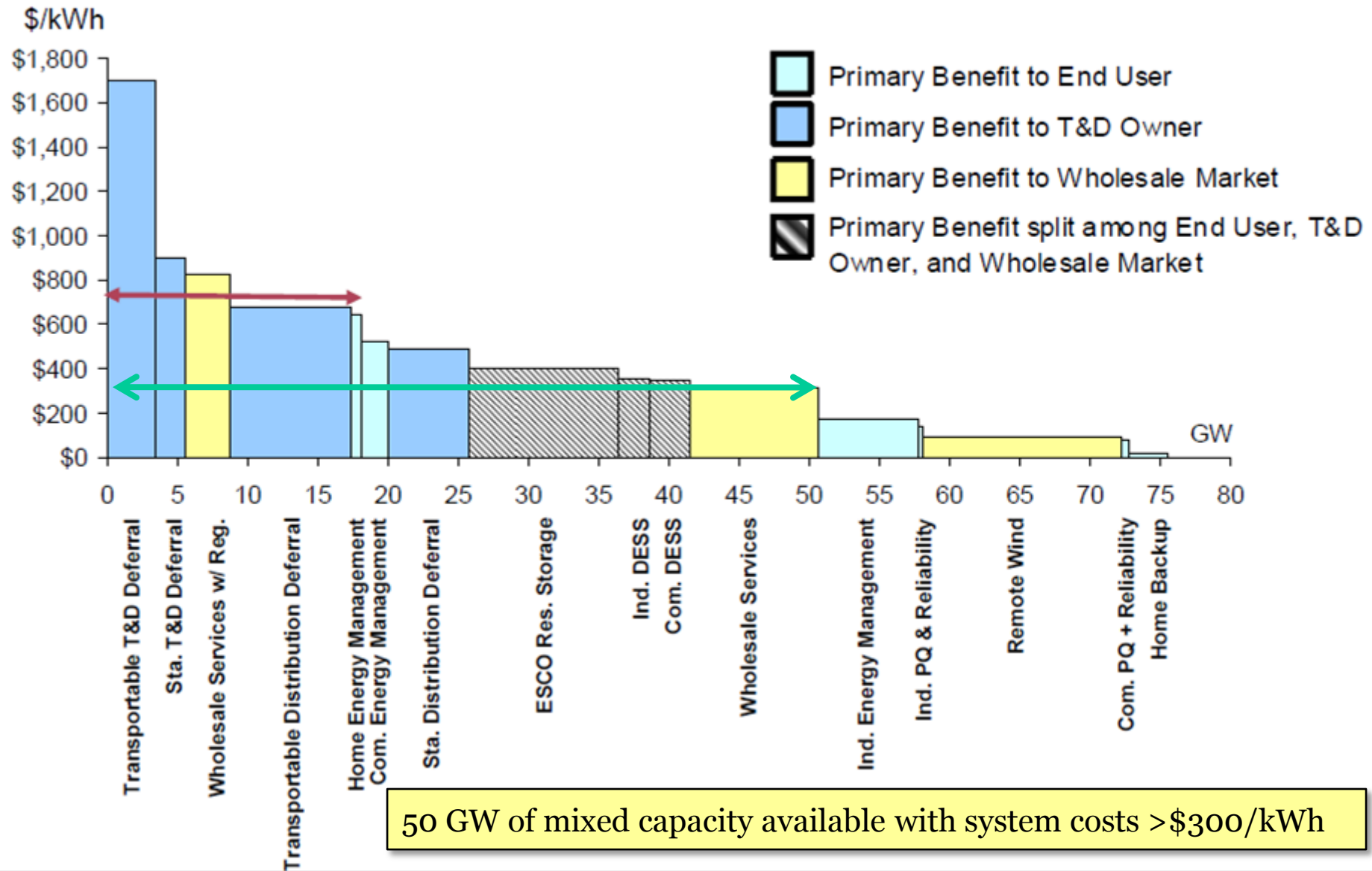


### metrics for grid-scale storage:

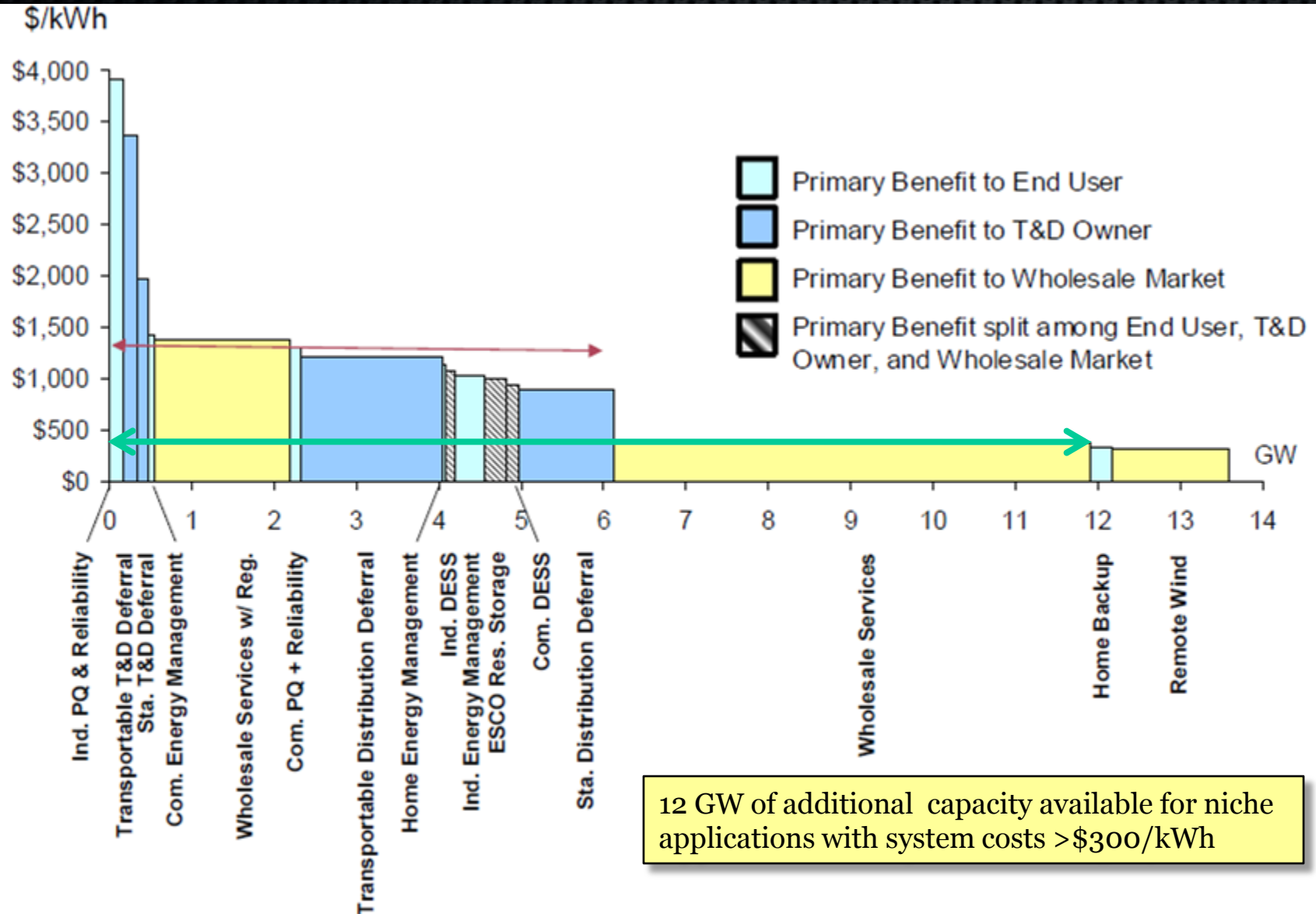
1. cost (< \$150/kWh)
2. lifespan (> 10 years)
3. energy efficiency (> 80 %)



# grid-level markets



# niche markets





# thought experiment



$C/2$  for PHEV  
 $C/12$  for EV



auto @ 45 mph  
electric motor ~ 10A



auto accelerates to 70mph  
electric motor ~ 100A

$4C$  for PHEV  
 $0.8C$  for EV



auto @ 70mph climbs hill  
electric motor ~ 300A

PHEV

BEV

40 mile range  
1.6 kWh  $\rightarrow$  8 mi

200 mile range  
5x energy

8kWh battery  
25 Ah @ 300V

40kWh battery  
125Ah @ 300V

high rate discharge  
critical for PHEV

not as critical for EV



$12C$  for PHEV  
 $2.5C$  for EV



# thought experiment



$C/2$  for PHEV  
 $C/12$  for EV



auto @ 45 mph  
electric motor ~ 10A



auto accelerates to 70mph  
electric motor ~ 100A

$4C$  for PHEV  
 $0.8C$  for EV



auto @ 70mph climbs hill  
electric motor ~ 300A

PHEV

BEV

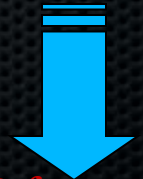
40 mile range  
1.6 kWh  $\rightarrow$  8 mi

200 mile range  
5x energy

8kWh battery  
25 Ah @ 300V

40kWh battery  
125Ah @ 300V

high rate discharge  
critical for ~~PHEV~~  
regulation  
not as critical for ~~EV~~  
bulk



$12C$  for PHEV  
 $2.5C$  for EV



# liquid metal battery



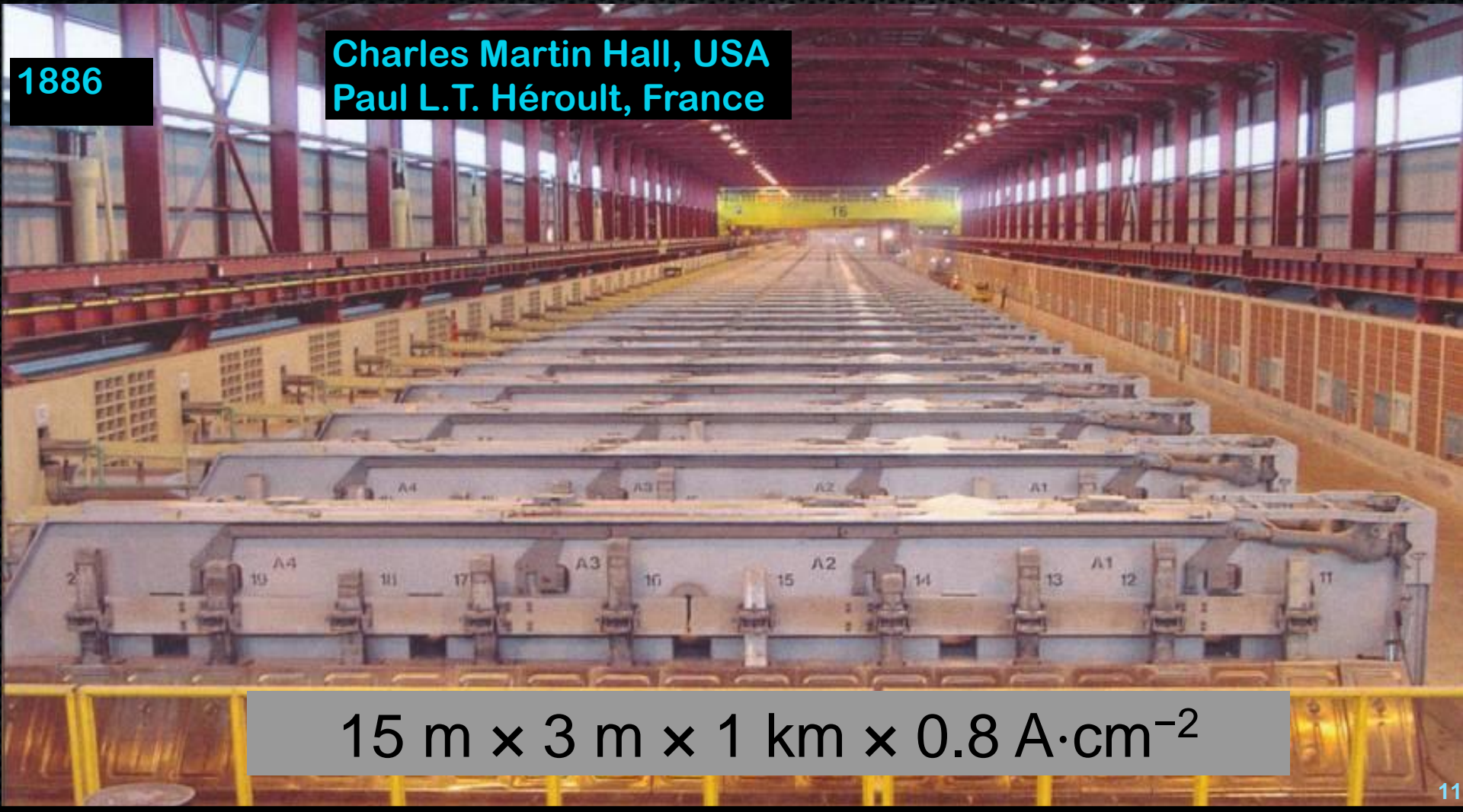
**Donald R. Sadoway**



**David J. Bradwell**



# a modern aluminium smelter



1886

Charles Martin Hall, USA  
Paul L.T. Hérault, France

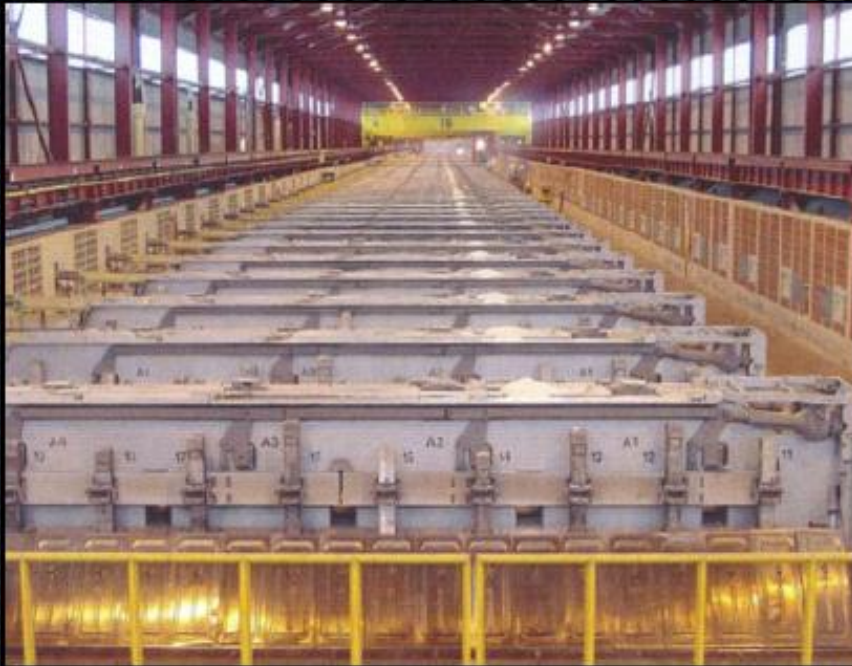
$15 \text{ m} \times 3 \text{ m} \times 1 \text{ km} \times 0.8 \text{ A} \cdot \text{cm}^{-2}$



key to finding the answer: pose the right question

different approach: find a giant current sink

convert this...



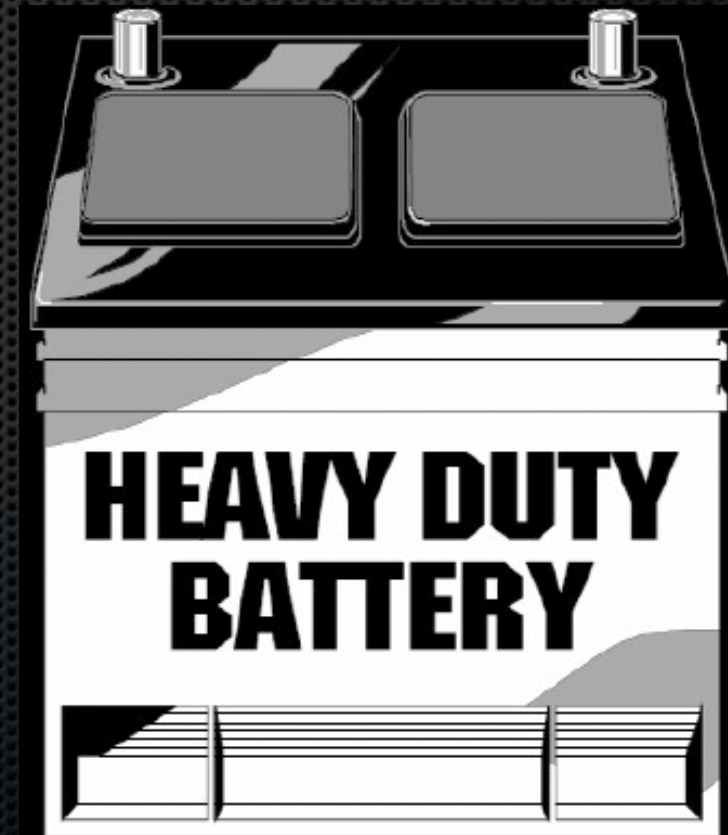
aluminum potline

350,000A ; 4V

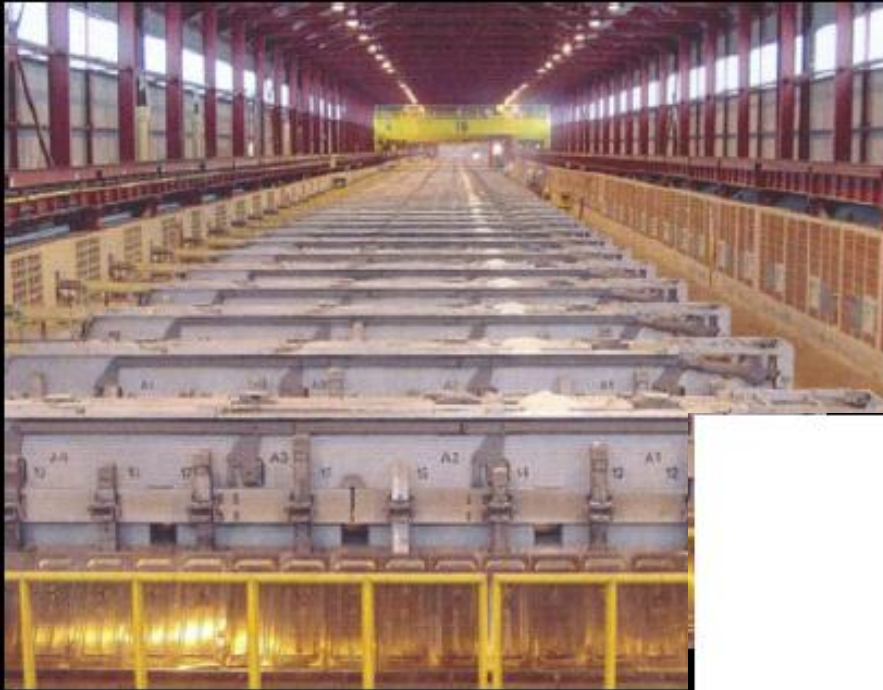
multiple MW per cell



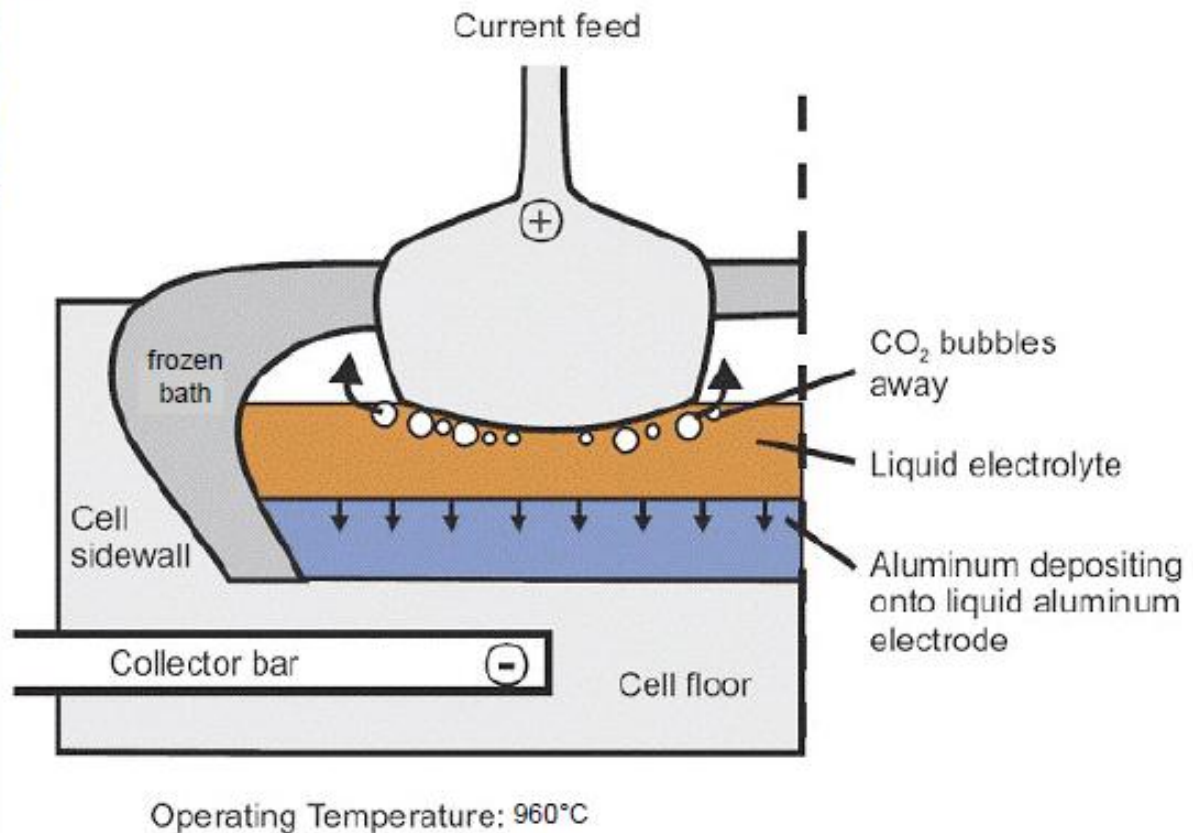
... into this







why is an aluminum cell not a battery?



👉 produce liquid metals at **BOTH** electrodes



# The Periodic Table of the Elements

*metals*  
*What about these?*

1 H Hydrogen	2 He Helium																	3 Li Lithium	4 Be Beryllium	5 B Boron	6 C Carbon	7 N Nitrogen	8 O Oxygen	9 F Fluorine	10 Ne Neon	11 Na Sodium	12 Mg Magnesium	13 Al Aluminum	14 Si Silicon	15 P Phosphorus	16 S Sulfur	17 Cl Chlorine	18 Ar Argon	19 K Potassium	20 Ca Calcium	21 Sc Scandium	22 Ti Titanium	23 V Vanadium	24 Cr Chromium	25 Mn Manganese	26 Fe Iron	27 Co Cobalt	28 Ni Nickel	29 Cu Copper	30 Zn Zinc	31 Ga Gallium	32 Ge Germanium	33 As Arsenic	34 Se Selenium	35 Br Bromine	36 Kr Krypton	37 Rb Rubidium	38 Sr Strontium	39 Y Yttrium	40 Zr Zirconium	41 Nb Niobium	42 Mo Molybdenum	43 Tc Technetium	44 Ru Ruthenium	45 Rh Rhodium	46 Pd Palladium	47 Ag Silver	48 Cd Cadmium	49 In Indium	50 Sn Tin	51 Sb Antimony	52 Te Tellurium	53 I Iodine	54 Xe Xenon	55 Cs Cesium	56 Ba Barium	57 La Lanthanum	58 Ce Cerium	59 Pr Praseodymium	60 Nd Neodymium	61 Pm Promethium	62 Sm Samarium	63 Eu Europium	64 Gd Gadolinium	65 Tb Terbium	66 Dy Dysprosium	67 Ho Holmium	68 Er Erbium	69 Tm Thulium	70 Yb Ytterbium	71 Lu Lutetium	72 Hf Hafnium	73 Ta Tantalum	74 W Tungsten	75 Re Rhenium	76 Os Osmium	77 Ir Iridium	78 Pt Platinum	79 Au Gold	80 Hg Mercury	81 Tl Thallium	82 Pb Lead	83 Bi Bismuth	84 Po Polonium	85 At Astatine	86 Rn Radon	87 Fr Francium	88 Ra Radium	89 Ac Actinium	90 Th Thorium	91 Pa Protactinium	92 U Uranium	93 Np Neptunium	94 Pu Plutonium	95 Am Americium	96 Cm Curium	97 Bk Berkelium	98 Cf Californium	99 Es Einsteinium	100 Fm Fermium	101 Md Mendelevium	102 No Nobelium	103 Lr Lawrencium
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24.3050

12

2

650

1090

1.74

1.31

7.646

[Ne]3s<sup>2</sup>

Magnesium

Mg

74.92159

33

±3,5

817TP

614SP

5.727<sup>25°C</sup>

2.18

9.81

[Ar]3d<sup>10</sup>4s<sup>2</sup>p<sup>3</sup>

Arsenic

As

78.96

34

-2,4,6

221

685

4.81

2.55

9.752

[Ar]3d<sup>10</sup>4s<sup>2</sup>p<sup>4</sup>

Selenium

Se

121.757

51

±3,5

630.63

1587

6.684<sup>25°C</sup>

2.05

8.641

[Kr]4d<sup>10</sup>5s<sup>2</sup>p<sup>3</sup>

Antimony

Sb

127.60

52

-2,4,6

449.51

988

6.25

2.1

9.009

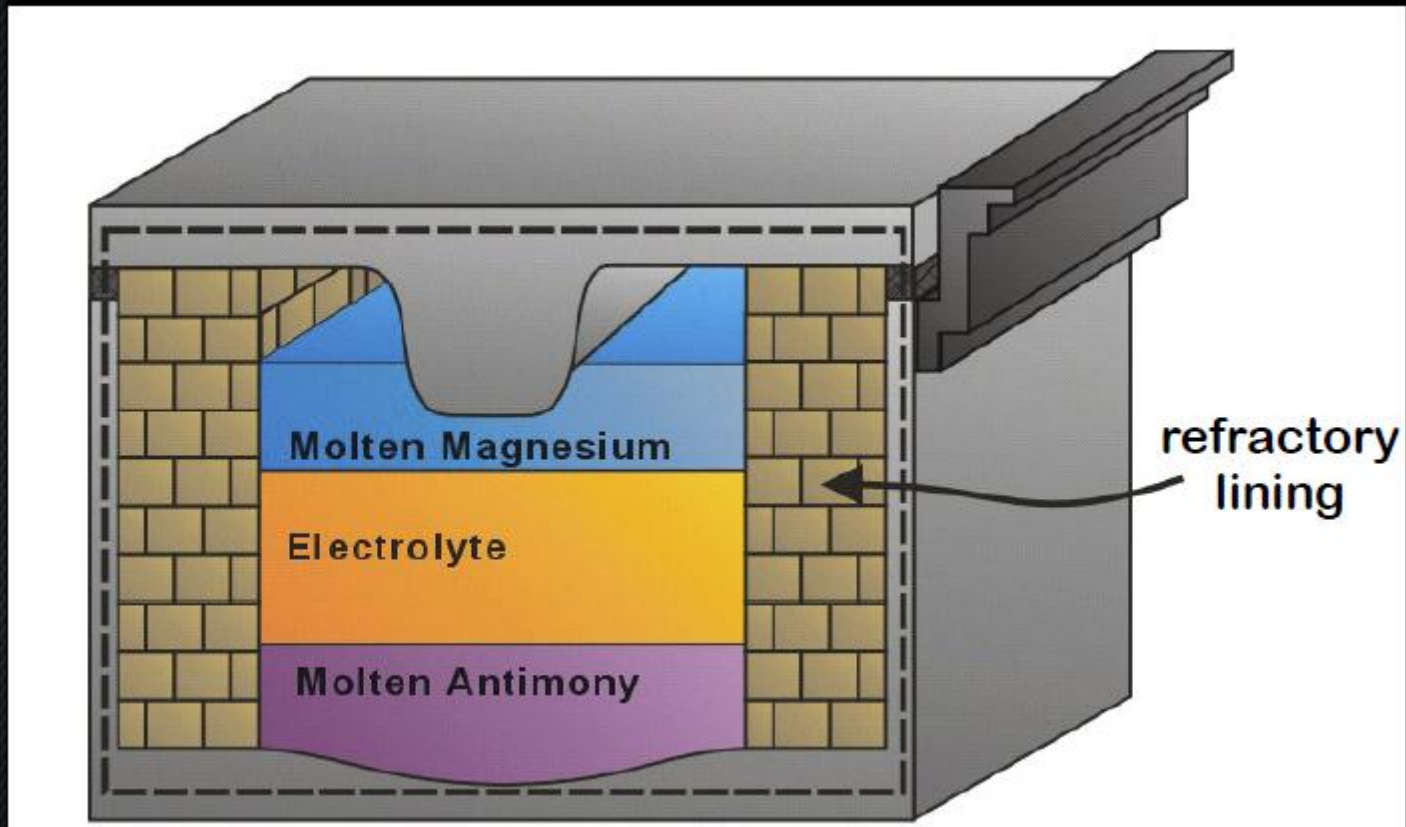
[Kr]4d<sup>10</sup>5s<sup>2</sup>p<sup>4</sup>

Tellurium

Te

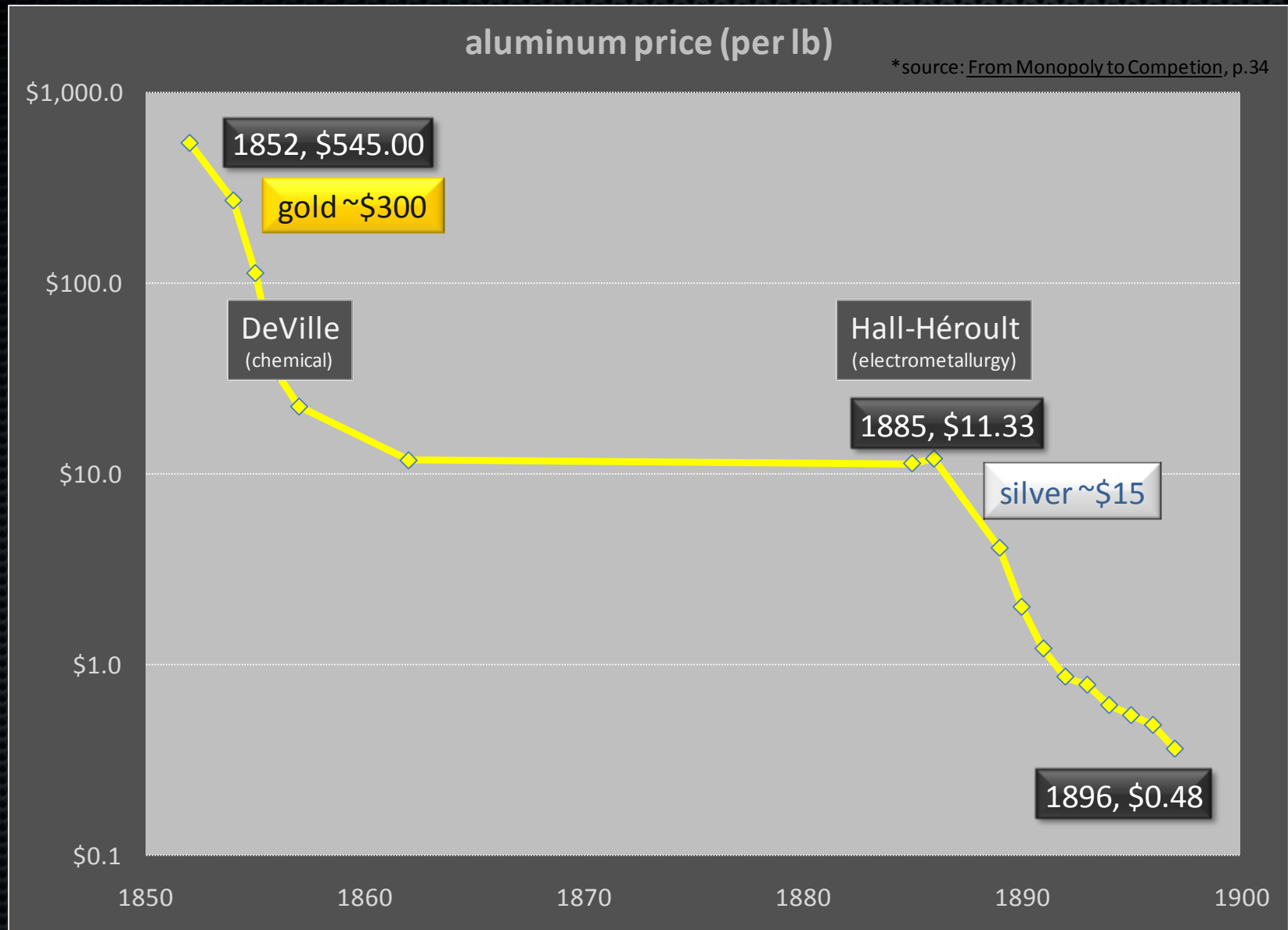


# ambipolar electrolysis on discharge





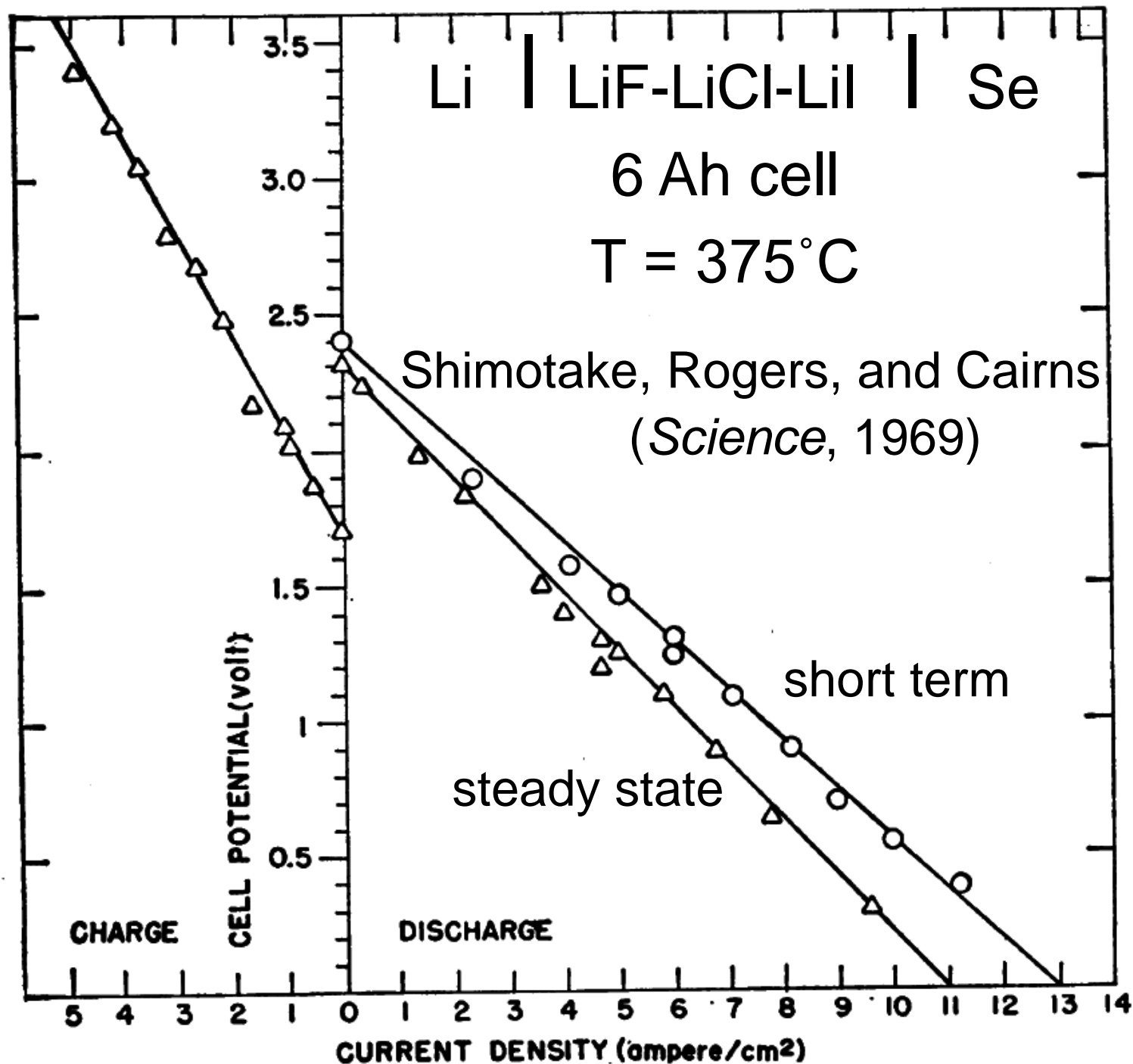
# economies of scale in electrometallurgy



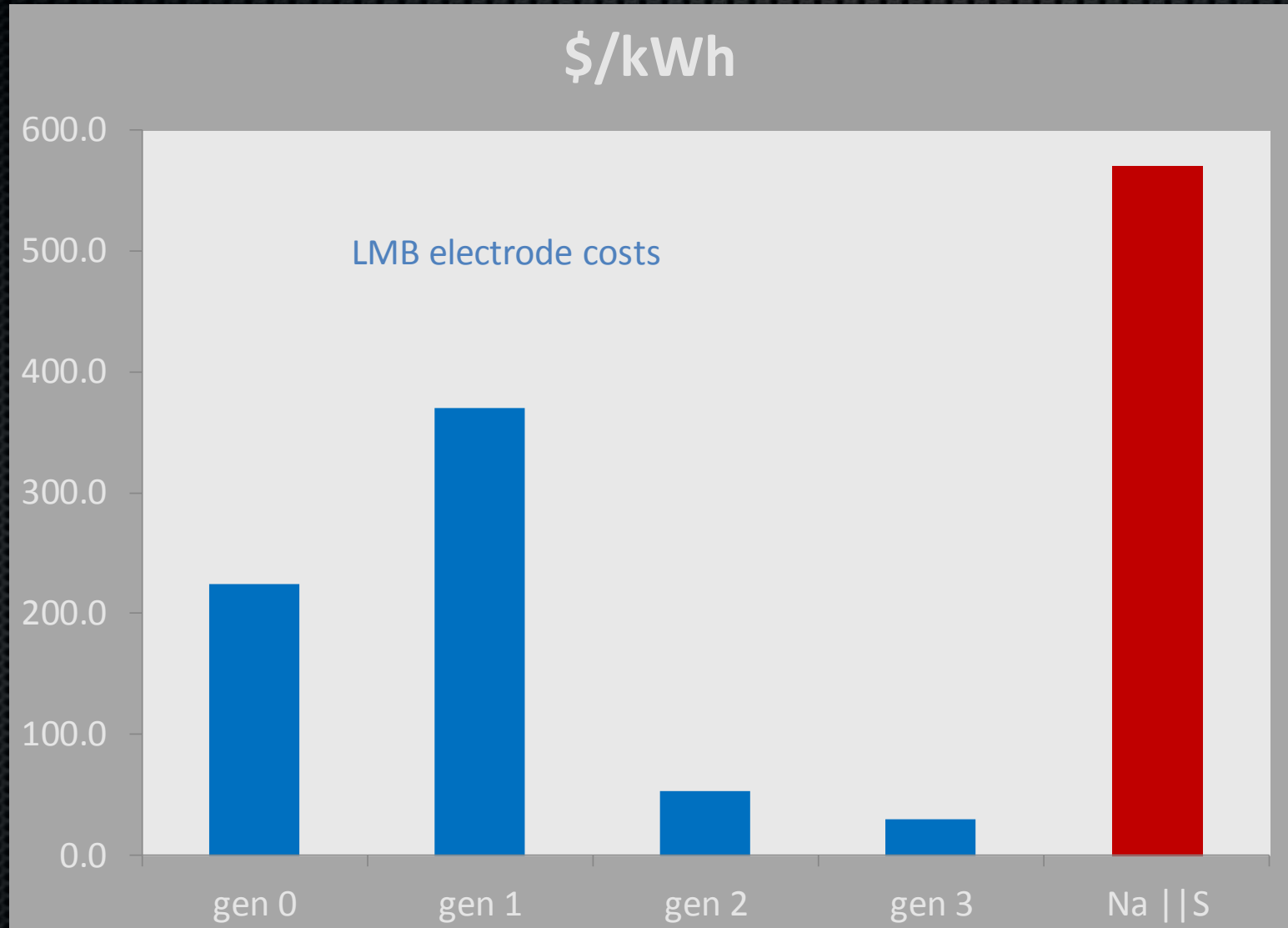
# attributes of a liquid state battery

- ◉ liquid-liquid interfaces are kinetically the fastest in all of electrochemistry
  - ☞ low activation overvoltage
- ◉ all-liquid construction eliminates any reliance on solid-state diffusion
  - ☞ long service life
- ◉ all-liquid configuration is self-assembling
  - ☞ scalable at low cost





# ARPA-e project





# ARPA-e development plan

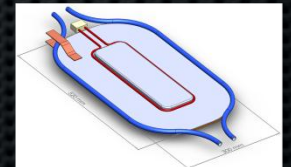
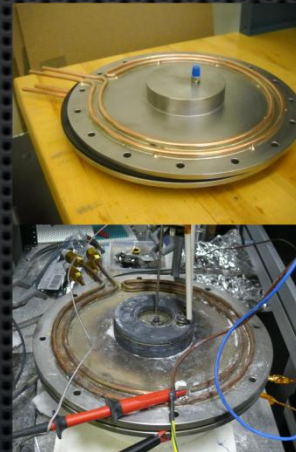
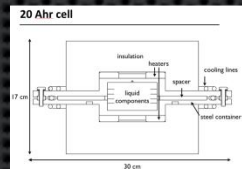
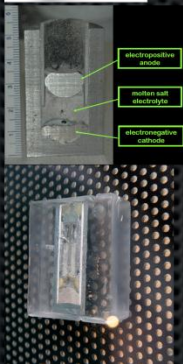
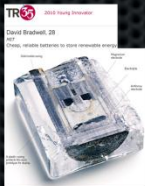
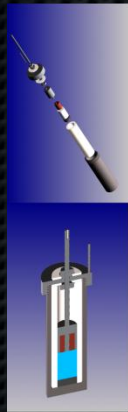
1 Ah



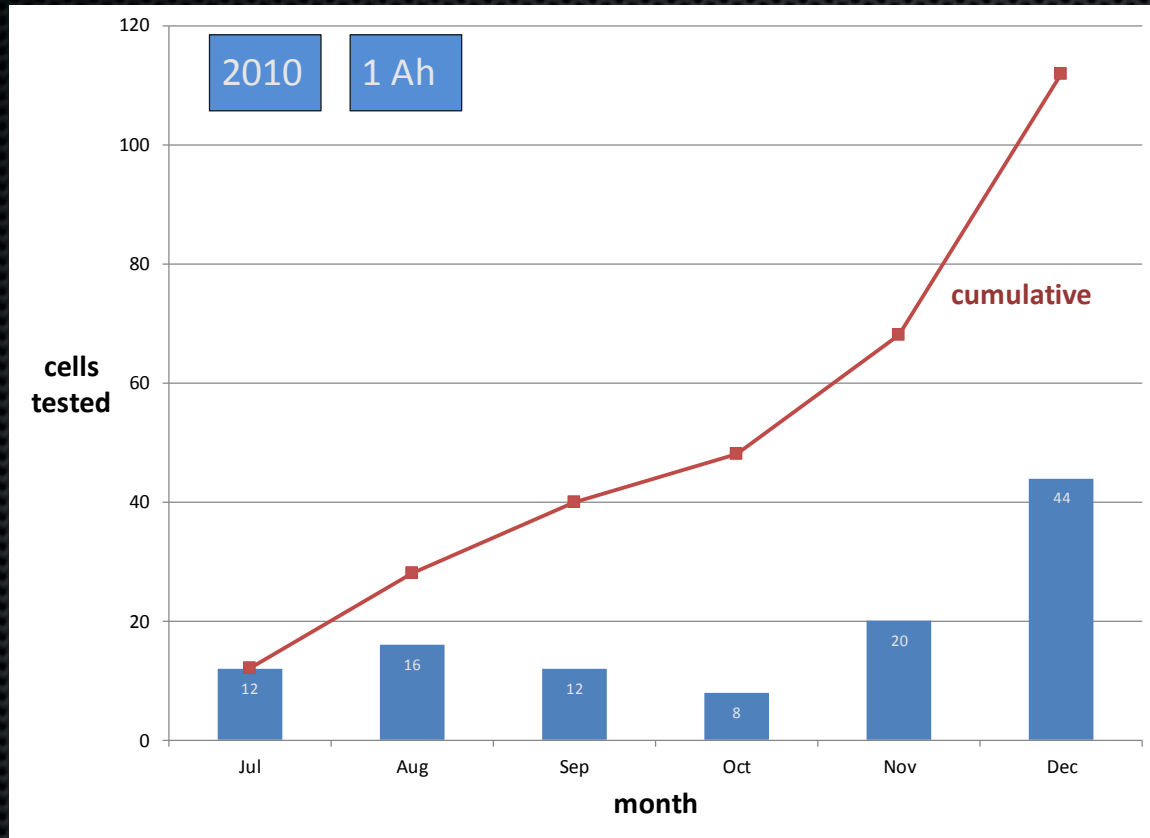
20 Ah



200 Ah



# technology maturity

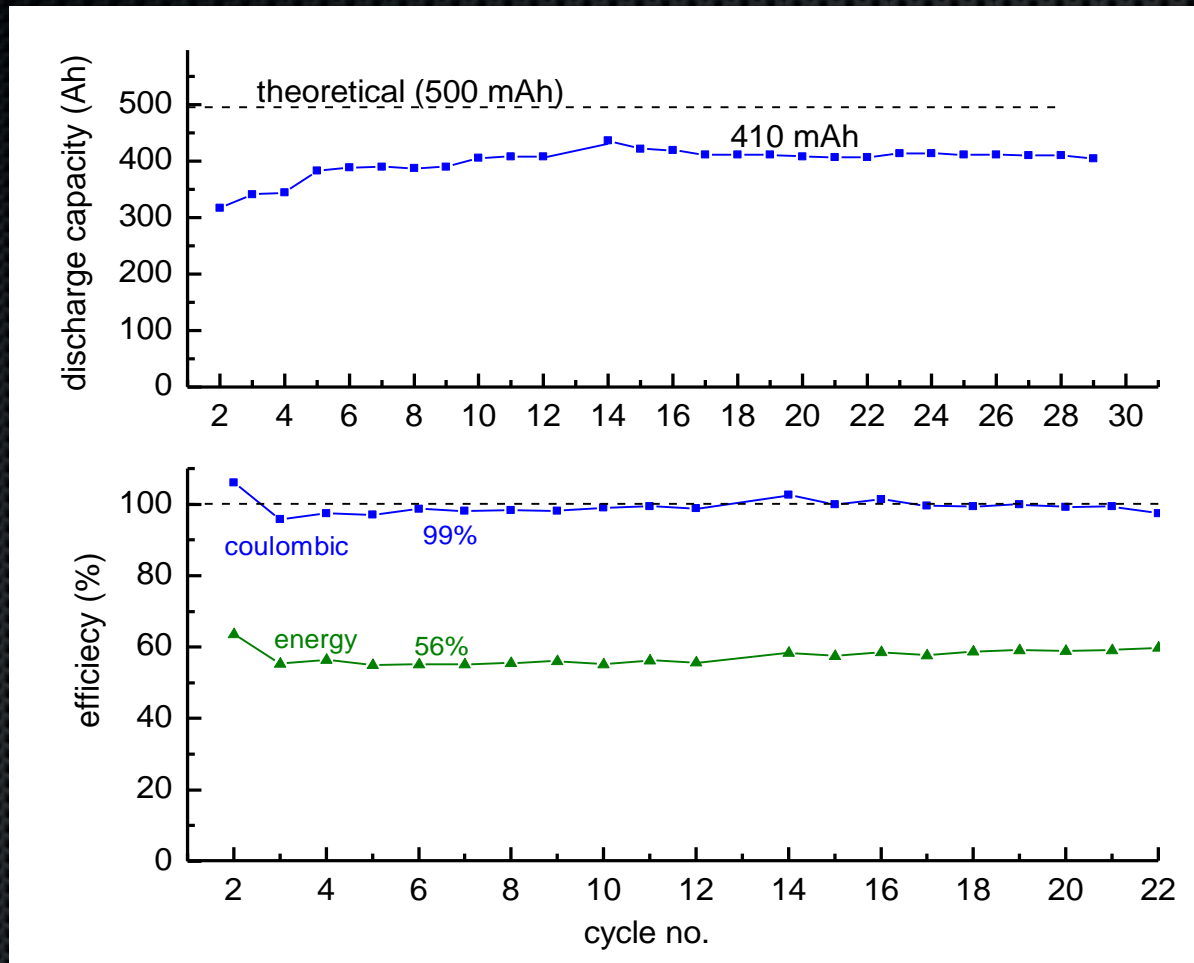




# 1 Ah cell performance

Metric	'Best of' cell results
1. Discharge capacity	650 mAh/cm <sup>2</sup>
2. Nominal discharge voltage	0.68 V @ 250 mA/cm <sup>2</sup>
3. Capacity fade	0 %/cycle
4. Round-trip energy efficiency	65 %
5. Electrode cost	\$ 81 /kWh; \$ 210 /kW

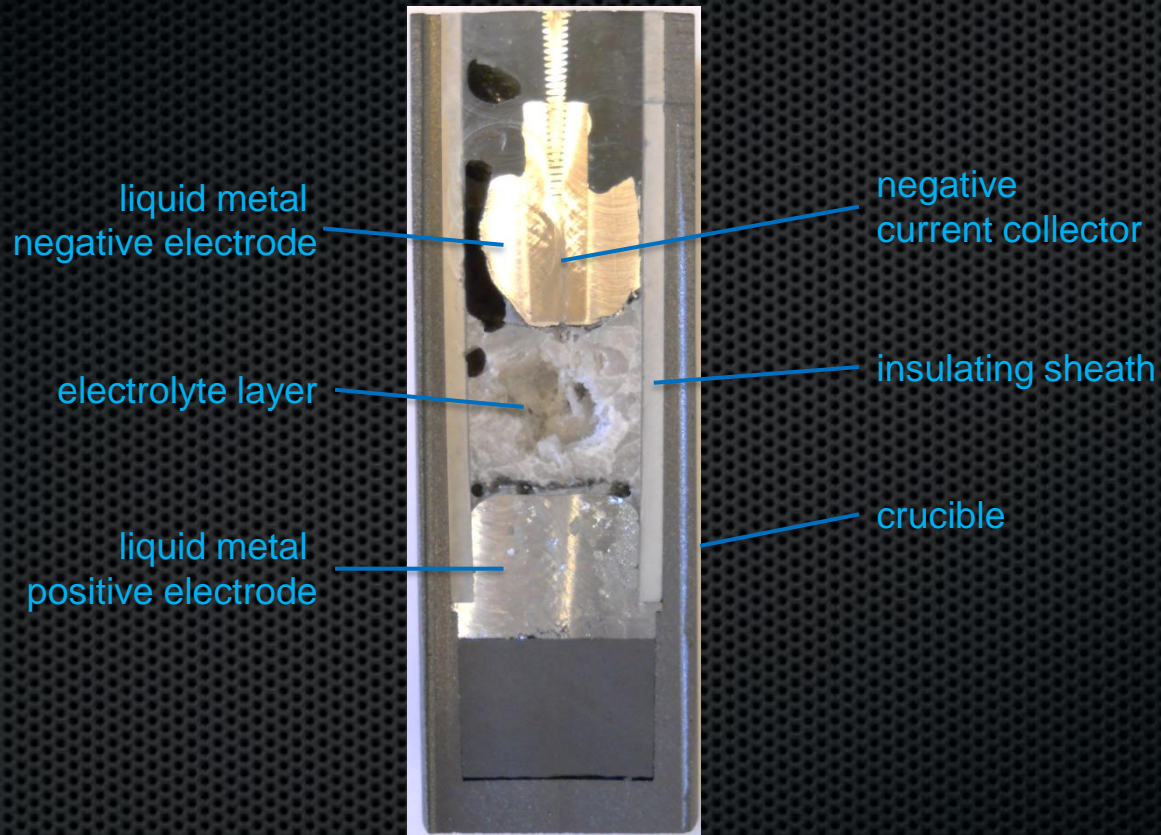
# 1 Ah cell performance



Capacity and efficiency performance data as a function of cycle number.  
*Note: energy efficiency can be improved by electrolyte optimization. Energy efficiency values of > 70 % have been achieved in other cells.*

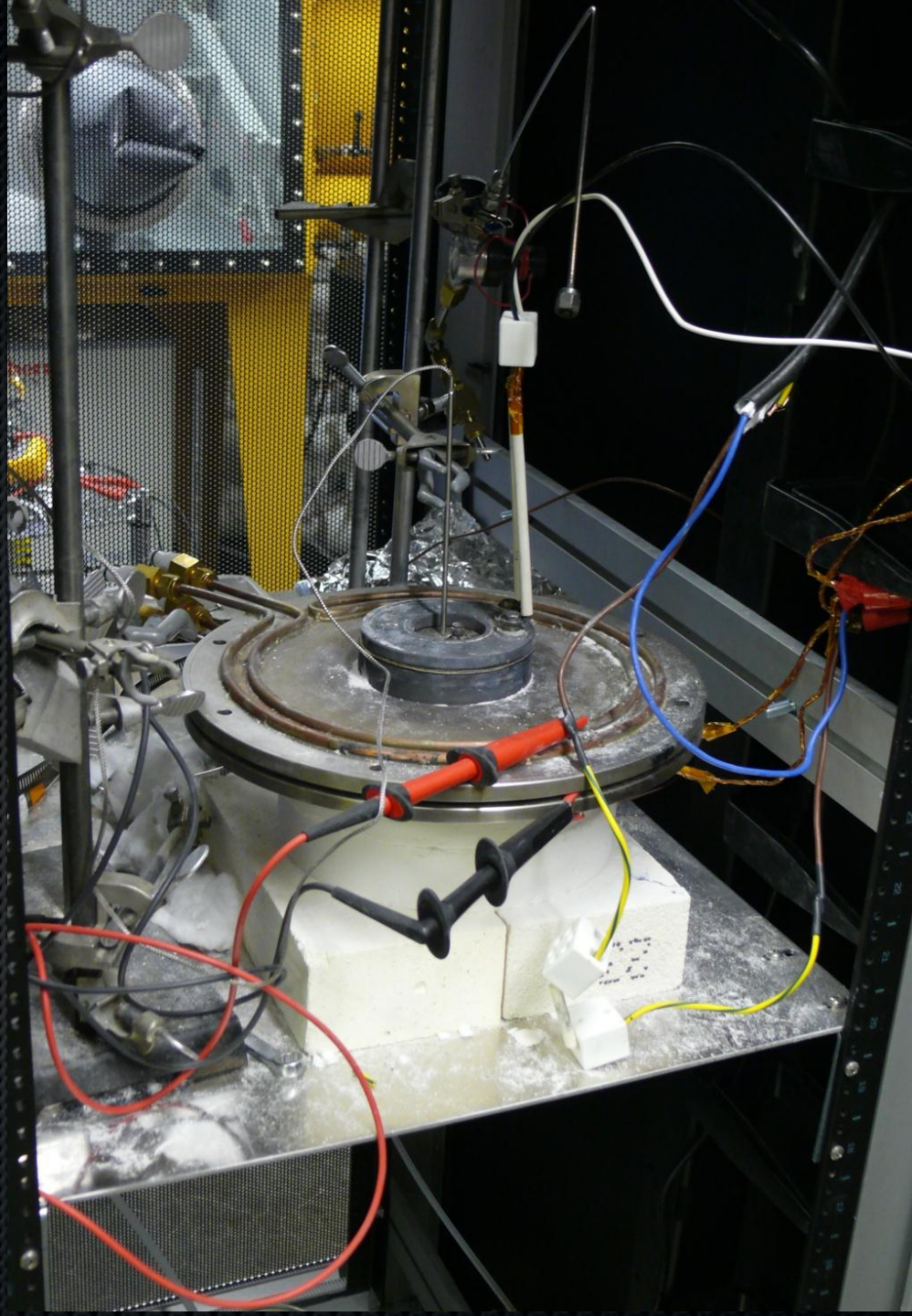


# 1 Ah cell cross section

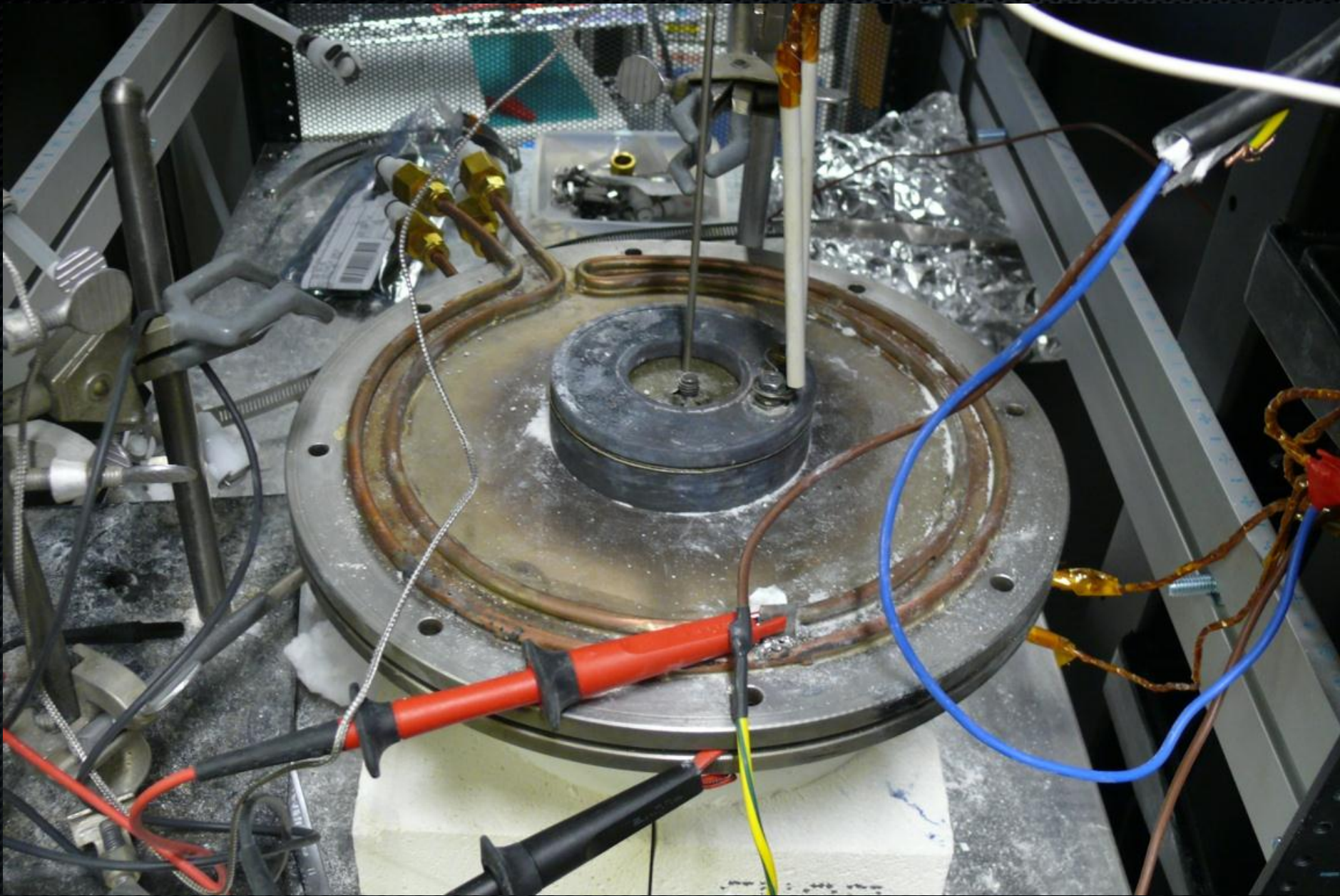


*This is an example of a cross sectioned liquid metal battery. Although the component are liquid at room temperature, the two metal electrodes and electrolyte layers are all liquid during operation.*

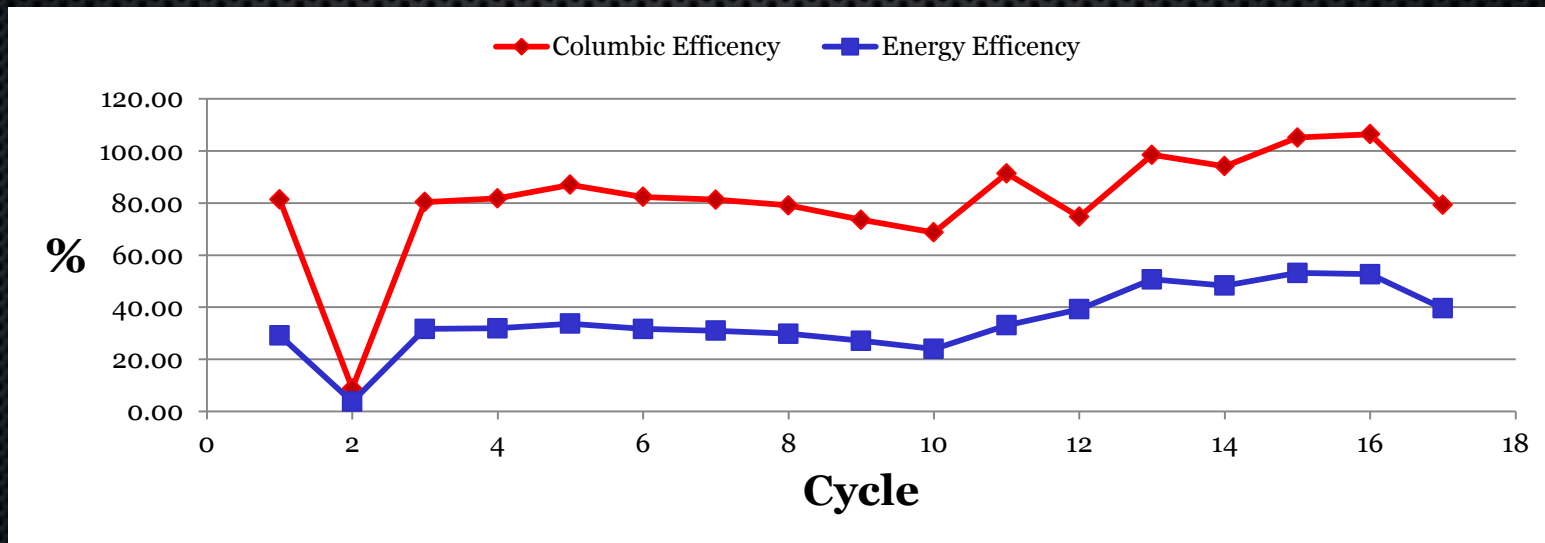
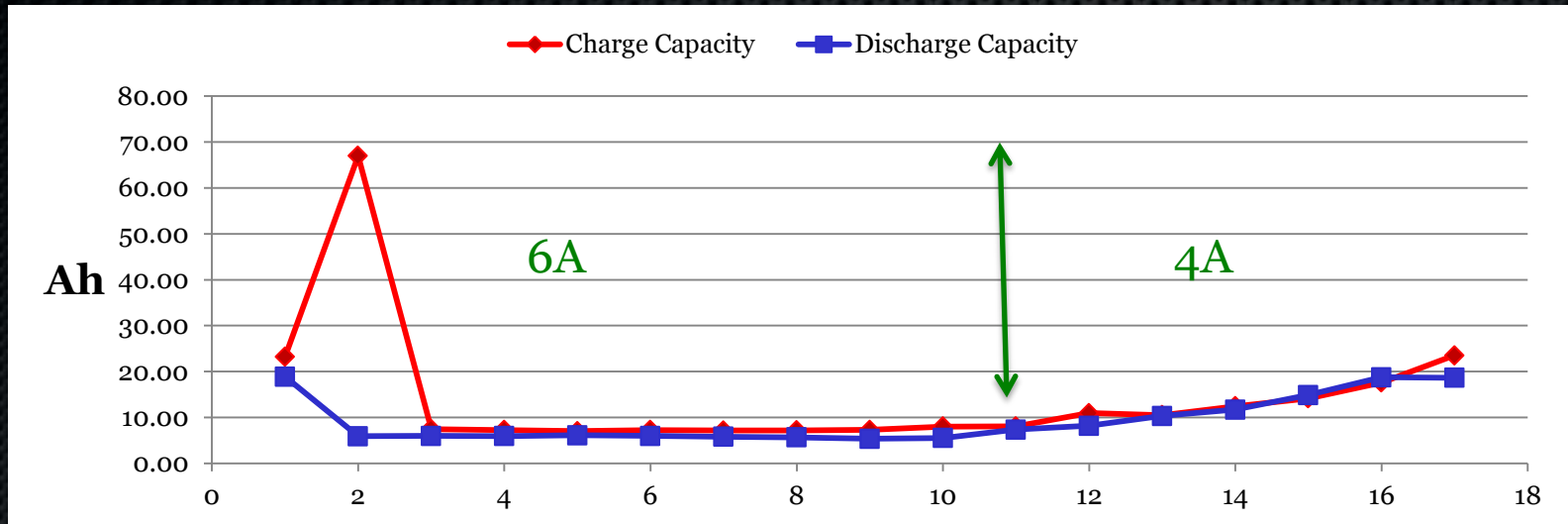






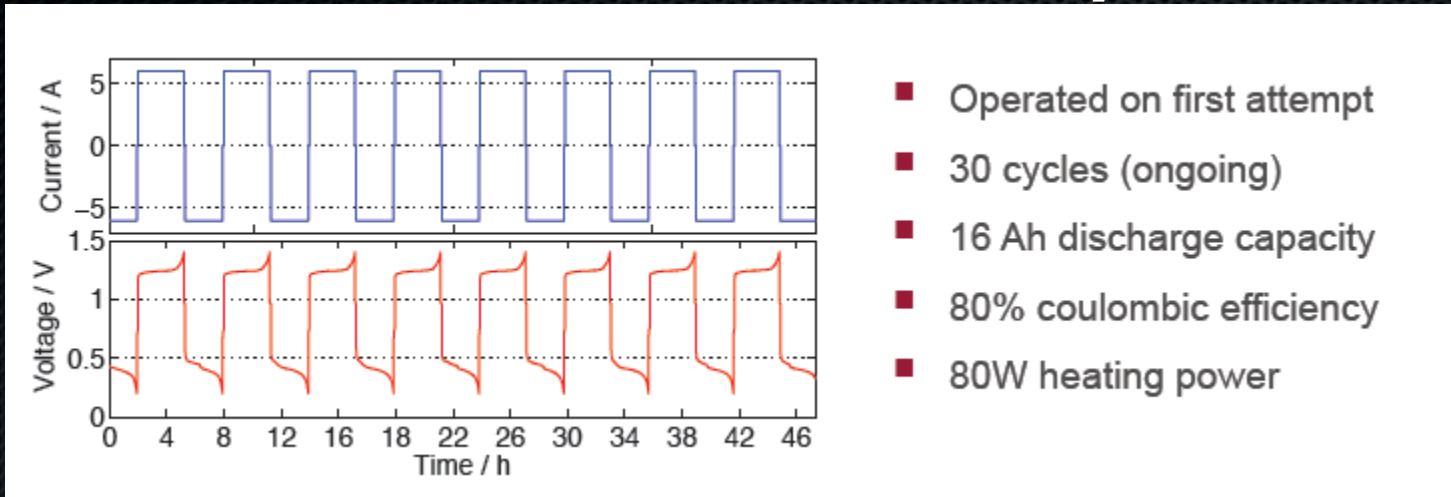


# 20 Ah cell cycling





# 20 Ah summary



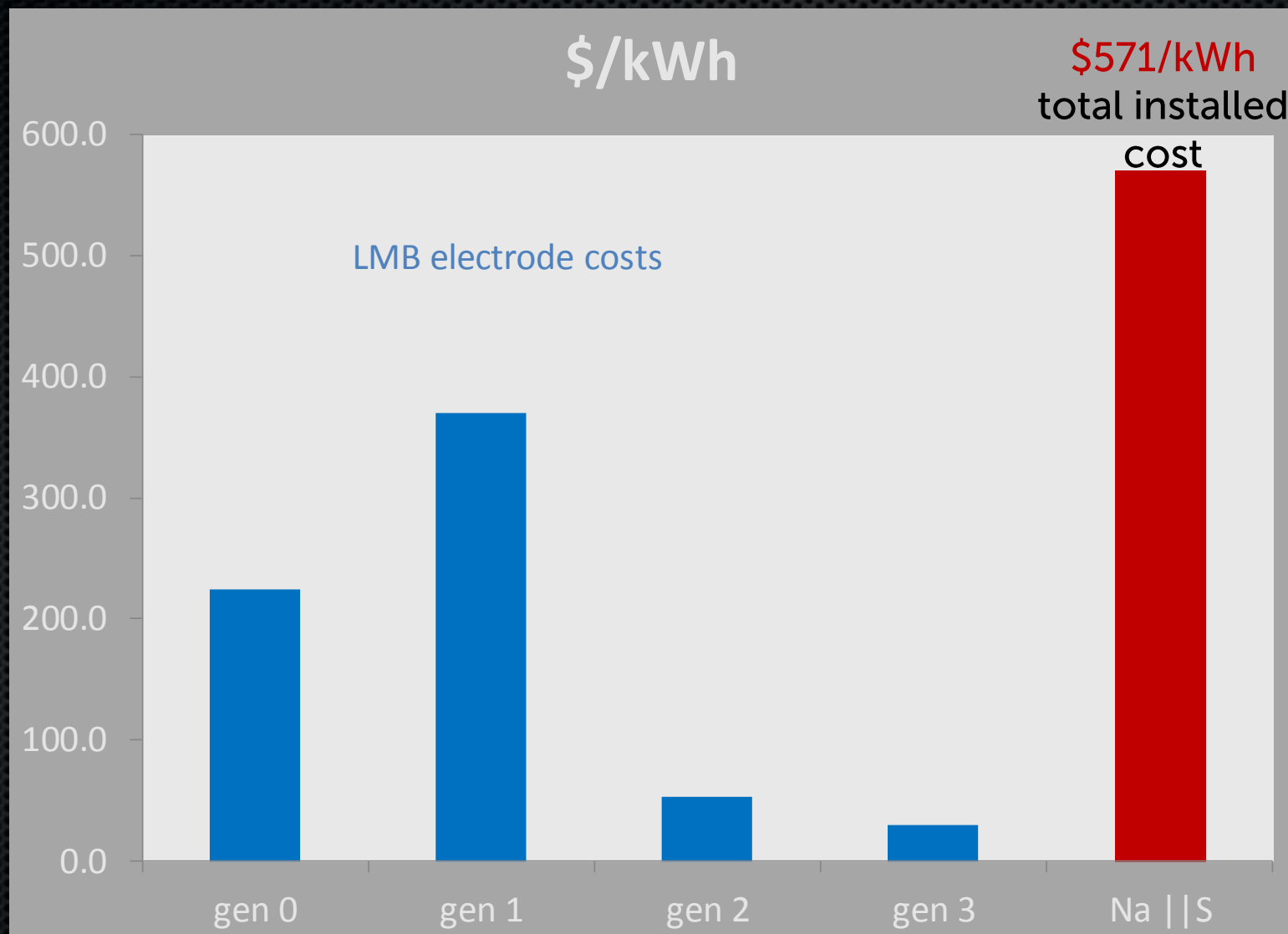
- ◉ 3 weeks continuous cycling (on going)
- ◉ 70 cycles
- ◉ comparable to ANL performance (17 months continuous no fade or degradation)
- ◉ electrolyte not optimized → practical system will have improved efficiency

"The storage battery is, in my opinion, a catchpenny, a sensation, a mechanism for swindling the public by stock companies. The storage battery is one of those peculiar things which appeals to the imagination, and no more perfect thing could be desired by stock swindlers than that very selfsame thing. ... Just as soon as a man gets working on the secondary battery it brings out his latent capacity for lying. ... Scientifically, storage is all right, but, commercially, as absolute a failure as one can imagine."

THOMAS EDISON in The Electrician (London) February 17, 1883, pp. 329-331 as quoted in Bottled Energy: Electrical Engineering and the Evolution of Chemical Energy Storage by Richard H. Schallenberg



# costs



# cost estimation

- ◉ LMB is believed not only to have low materials costs, but also economies of scale upon commercialization
- ◉ basis: intuition & analysis
- ◉ four (4) MIT masters theses
  - ☞ original analysis justifying initial research
  - ☞ NPV based analysis indicating need for multiple applications even when costs are low
  - ☞ top down 'retrofit' analysis of new build AL smelters which identified power electronics costs
  - ☞ recent analysis identifying electrolyte cost sensitivity



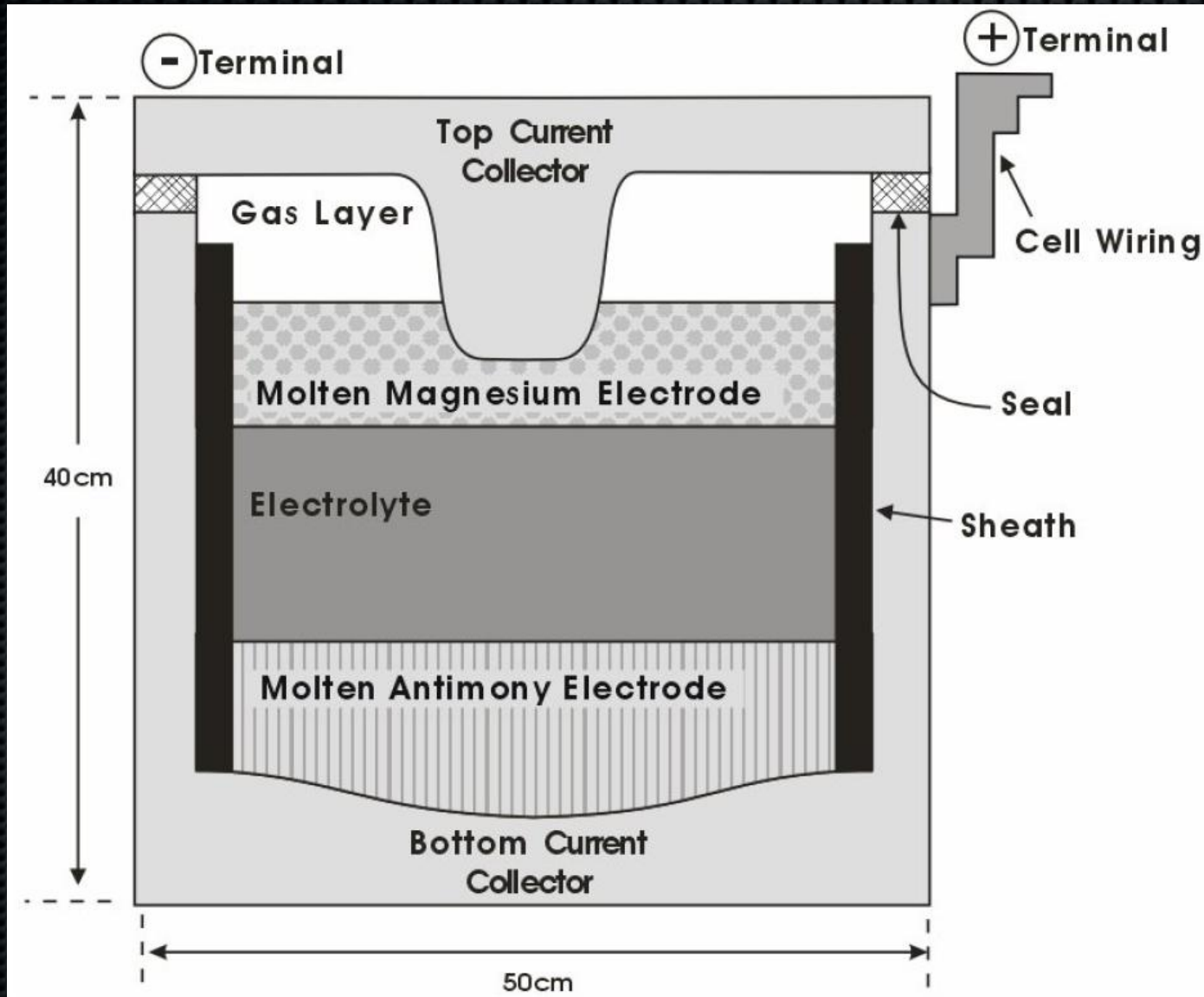
# masters thesis #1



David J. Bradwell

- ◉ bottom up analysis
- ◉ \$100/kWh as critical price metric for pure arbitrage application
- ◉ key information point for Deshpande Center funding

# cell concept

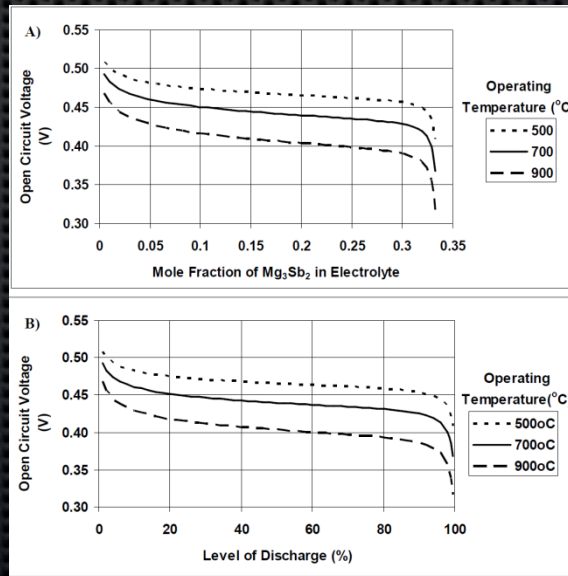




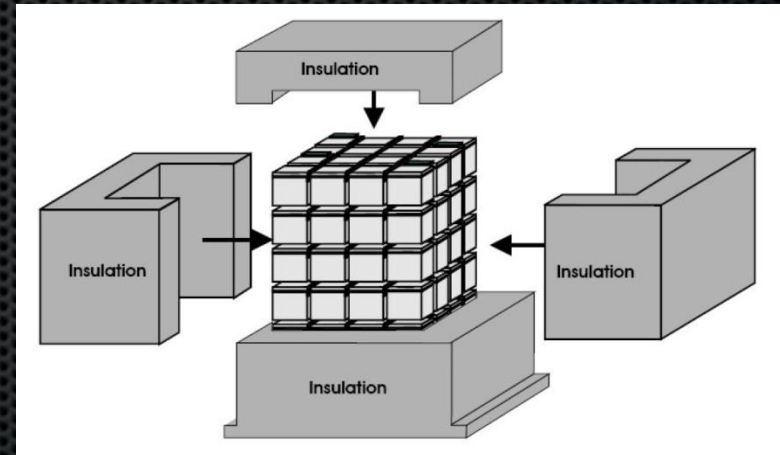
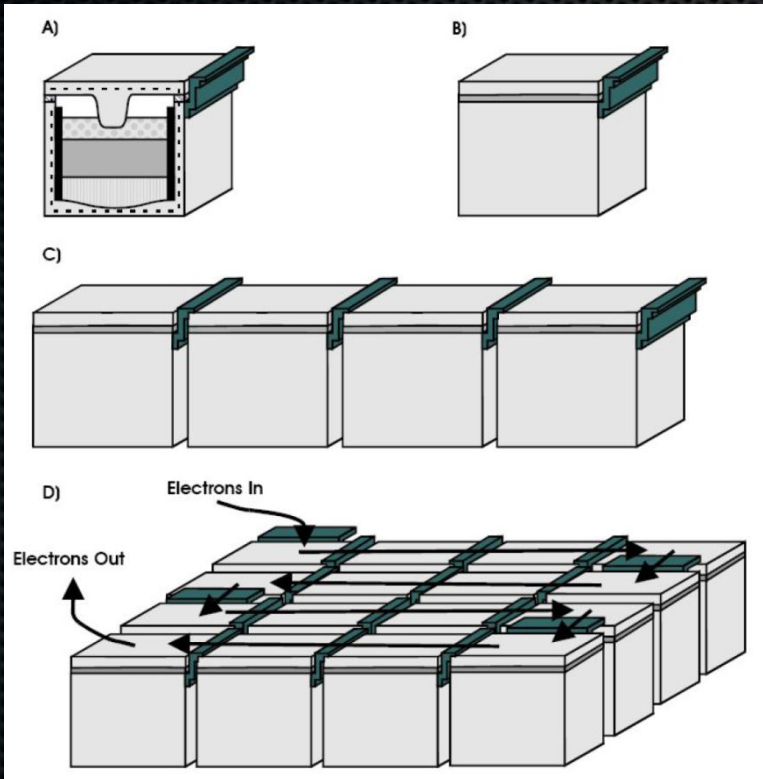
# battery performance estimates



Compound	Dissociation Potential, 700°C (V)	Compound	Dissociation Potential, 700°C (V)
Na <sub>2</sub> S	1.60	Li <sub>2</sub> S	1.97
Na <sub>2</sub> Te	1.35	Li <sub>2</sub> Se	1.87
Na <sub>2</sub> Se	1.20	Li <sub>2</sub> Te	1.60
Na <sub>3</sub> Sb	0.54 (?)	Li <sub>3</sub> Sb	0.9 (?)
Na <sub>3</sub> As	0.3 (?)	K <sub>2</sub> S	1.60
MgS	1.66	K <sub>3</sub> Sb	0.9 (?)
MgSe	1.30	K <sub>2</sub> Te	0.75 (?)
MgTe	1.00	CaS	2.30
<b>Mg<sub>3</sub>Sb<sub>2</sub></b>	<b>0.42</b>	CaSe	1.80
		CaTe	1.40
		Ca <sub>3</sub> Sb <sub>2</sub>	1.08 (?)

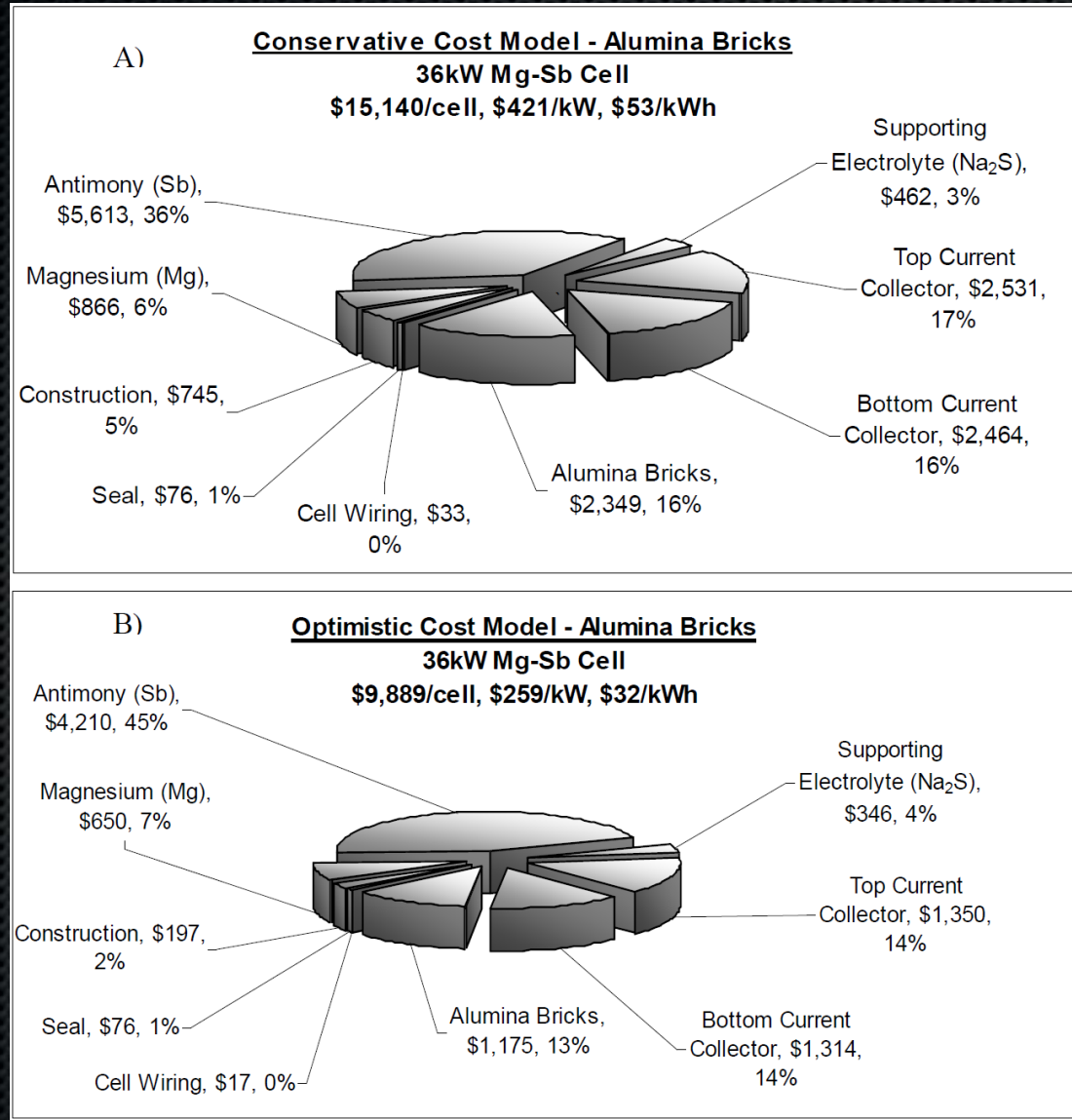


# proposed system





# cost estimate for 3m × 3m cell



# masters thesis #2



Ted A. Fernandez

- ◉ similar method of estimating system cost to thesis #1
- ◉ did a project based cost estimate and compared multiple storage technologies for each use case
- ◉ (nearly) all storage technologies could not produce an NPV break even in 15 years on a single use case
- ◉ stacking applications critical



# use cases



Use Profiles								
Application	Size	Duration	Response Time	Cycles	Roundtrip Efficiency	Lifetime	Depth of Discharge	Internal Losses
Renewable Off-Peak Storage	30 MW	6 hr	10 min	300/year	80%	10 years	90%	<5%
Ramp & Voltage Support	10 MW	2 hr	10 min	300/year	80%	10 years	90%	<5%
Time-of-Use & Demand Charge Management	1 MW	4 hr	10 seconds	300/year	80%	10 years	70 - 80 %	<5%
Mobile T&D Deferral (Upgrade Factor - .33%)*	4 MW	2 hr	10 min	300/year	80%	20 years	90%	<5%
Mobile T&D Deferral (Upgrade Factor - .50%)*	6 MW	2 hr	10 min	300/year	80%	20 years	90%	<5%

\*(From an initial 12MW)

# strategic analysis



Off-Peak Storage	Ramp & Voltage Support
Total energy Cycle life Scalability Max charge/discharge	Total energy Cycle life Lifetime Self discharge
Mobile T&D Deferral	TOU & Demand
Total energy Energy density Portability Plant footprint	Total energy Cycle life Energy Density Plant footprint

Specification Application	Total Energy per Cycle (kWh)	Cycle Life	Lifetime (years)	Energy Density	Scalability	Portability	Self Discharge	Max Charging Power % Above Rated Power	Annual Maintenan ce	Plant Footprint (kWh/m2)
Off-Peak Storage	●	●	●	●	●	●	○	●	○	○
Ramp & Voltage Support	●	●	●	●	●	●	●	○	●	○
Mobile Transmission & Deferral	●	●	●	●	●	●	○	●	○	●
TOU & Demand	●	●	●	●	●	●	○	○	●	●

Very important  Not important



# evaluation



Off-Peak Storage	Ramp & Voltage Support
<ul style="list-style-type: none"><li>LMB</li><li>Li-OP</li><li>NaS</li><li>LLLA</li><li>Flow Cell</li><li>Li-RE</li></ul>	<ul style="list-style-type: none"><li>NaS</li><li>LMB</li><li>Li-OP</li><li>LLLA</li><li>Li-RE</li><li>Flow Cell</li></ul>
Mobile T&D Deferral	TOU & Demand
<ul style="list-style-type: none"><li>Li-Op</li><li>LMB</li><li>NaS</li><li>Li-RE</li><li>Flow Cell</li><li>LLLA</li></ul>	<ul style="list-style-type: none"><li>LMB</li><li>Li-OP</li><li>LLLA</li><li>Li-RE</li><li>Flow Cell</li><li>NaS</li></ul>

# value for use cases



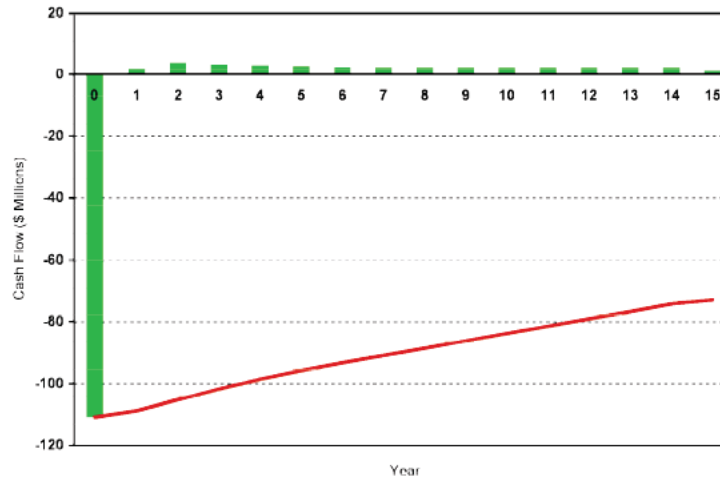
Renewable OPS	R&V Support	Mobile T&D (33%)
<b>\$54.2/kW-year</b>	<b>Low</b> <b>\$400/kW</b> (over 10 years) <b>High</b> <b>\$800/kW</b> (over 10 years)	<b>50th %ile</b> <b>\$684/kW-year</b>  <b>90th %ile</b> <b>\$1079/kW-year</b>
Mobile T&D (50%)	TOU & Demand	
<b>50th %ile</b> <b>\$1115/kW-year</b>  <b>90th %ile</b> <b>\$1821/kW-year</b>	<b>\$250.37/kW-year</b>	



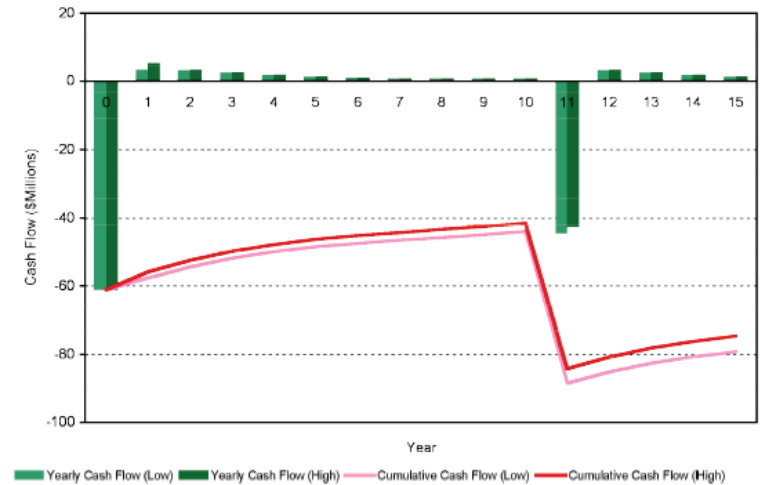
# project NPV analysis



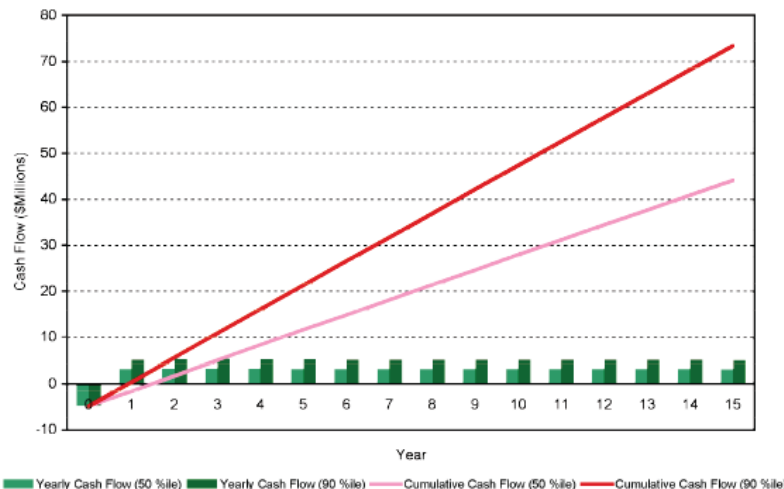
NAS - Off-Peak Storage Cash Flow



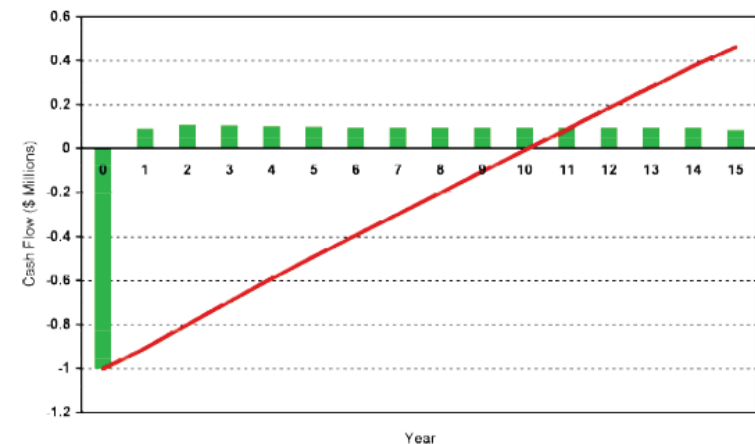
LI-RE - Ramp & Voltage Support Cash Flow



LMB-A - Mobile T&D (50% Upgrade) Cash Flow



LMB-B - TOU Cash Flow



# base analysis summary



	NAS	Flow	LLLA	Li-Op	Li-Re	LMB-A	LMB-B	LMB-C
Renewables Off-Peak Storage	●	●	●	●	●	●	●	●
Ramp & Voltage Support	●	●	●	●	●	●	●	●
Mobile T&D (33% Upgrade)	●	●	●	●	●	●	●	●
Mobile T&D (50% Upgrade)	●	●	●	●	●	●	●	●
TOU & Demand Charge Management	●	●	●	●	●	●	●	●

NPV > 0

NPV < 0; Break even < 15 years

Break even > 15 years



# summary



- ◉ two key drivers for project profitability
  - ☞ government incentives
  - ☞ stacking applications
- ◉ red and yellows turn green

# masters thesis #3

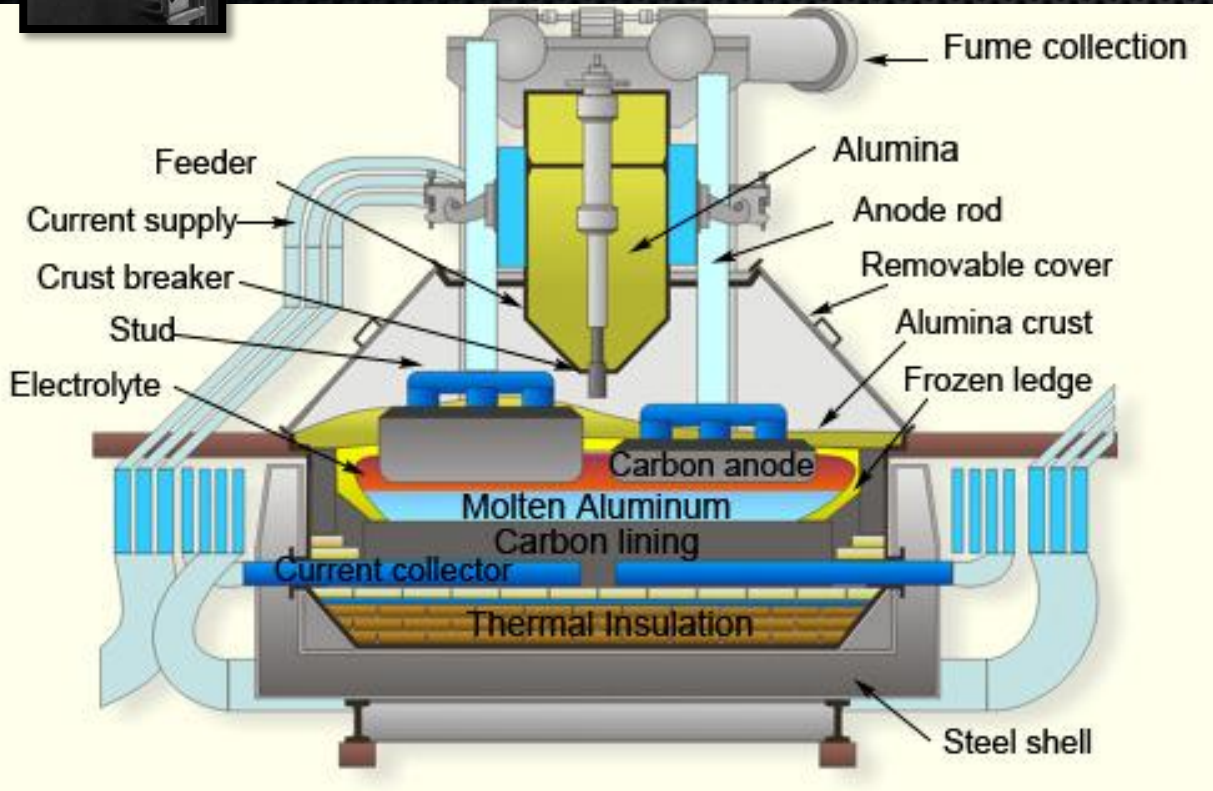


Isabel Garos

- used costs from most recent Al smelter
- eliminated unnecessary equipment and estimated cost of additional equipment
- modeled a 4 GWh battery in an area similar in size to a Walmart supercenter
- identified high current (100's of kA) inverter costs as a key cost leader at the system level



# Hall-Héroult cell



## AP35 Cell

Operating current: 350kA

Pot Size(approx): 10x3.5x1.2m

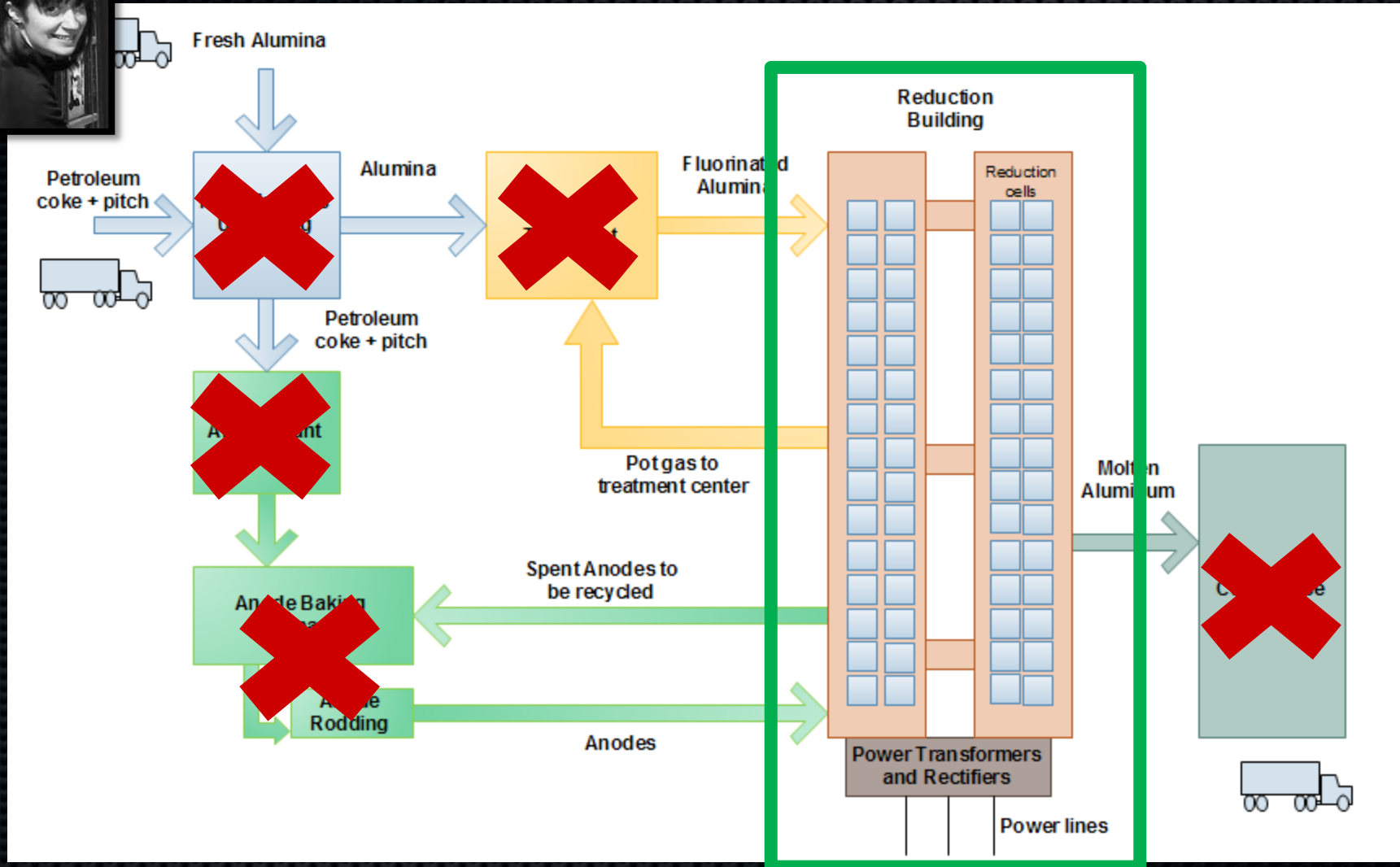
Production: 2.7 tons/pot/day

Consumption: 13,000 kWh/ton

Current efficiency: up to 95.1%

Working temperature: 960°C

# aluminum smelter





# smelter investment

## ○ Sohar Smelter:

☞ Location: Sohar, Oman

☞ Builder: Bechtel

☞ Commissioned in 2008



☞ Most advanced technology

☞ 360,000 tpy, \$2,000 million, \$5,500/tpy

☞ 360 AP35 pots; 350kA; 1,650Vdc

- 580MW 4.58V/cell

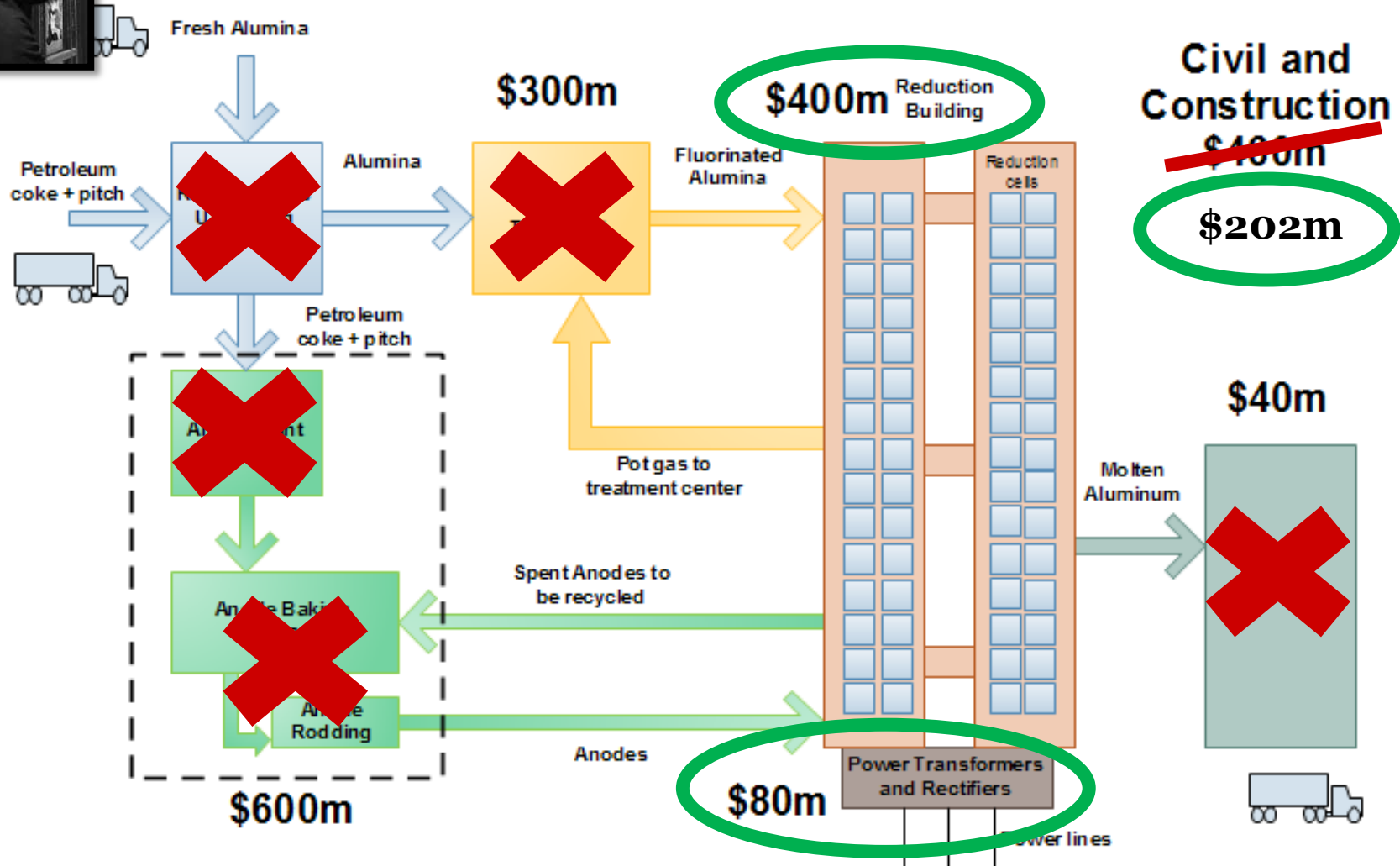
☞ 2 pot-rooms, 1km long each

- 180 pots per room

# investment breakdown

## 360 000 ton Smelter Cost Overview

Total: \$682 million





# base case



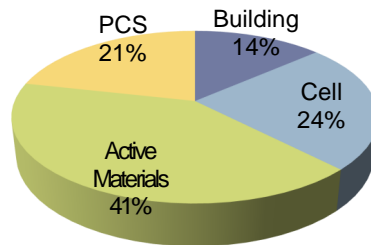
Cell design			
	Length	3.5	m
	Width	10	m
	Height	0.3	m
	Cell area	35	m <sup>2</sup>
Cell characteristics			
	Cell voltage	1	V
	Current density	1	A/cm <sup>2</sup>
	Total current	350	kA
	Cell efficiency	100%	
	Roundtrip efficiency	90%	
	Charge/discharge time	8	hours
	Cell power	350	kW
	Cell capacity	2800	kWh

LMB A	LMB B	LMB C
\$150/kWh	\$50/kWh	\$30/kWh

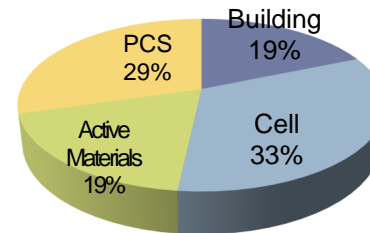
# base case: results



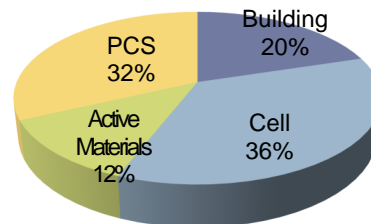
**LMB A, \$408.26/kWh**



**LMB B, \$297.15/kWh**



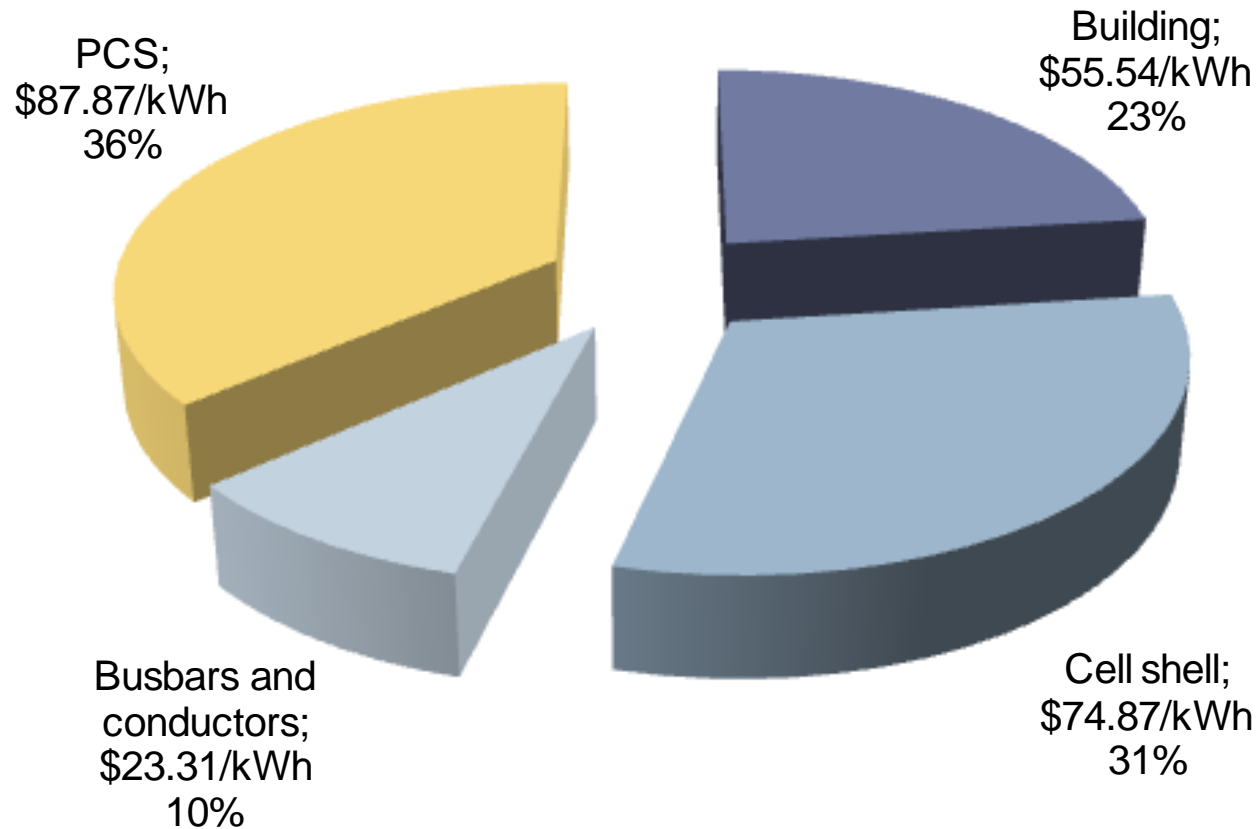
**LMB C, \$274.93/kWh**





# base case

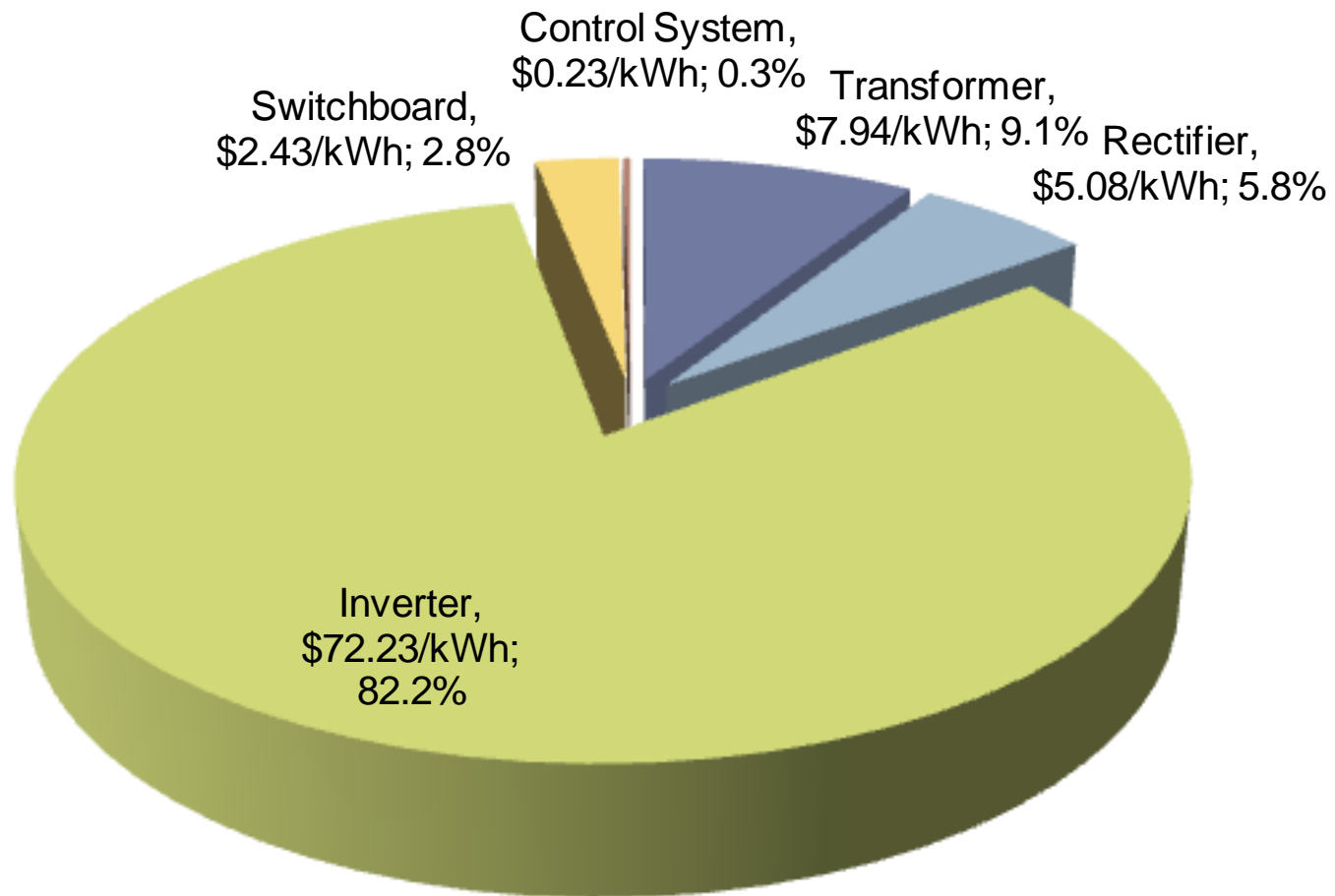
## Non-active materials cost \$241.6/kWh



# base case



## PCS Total cost \$87.88/kWh





# base case

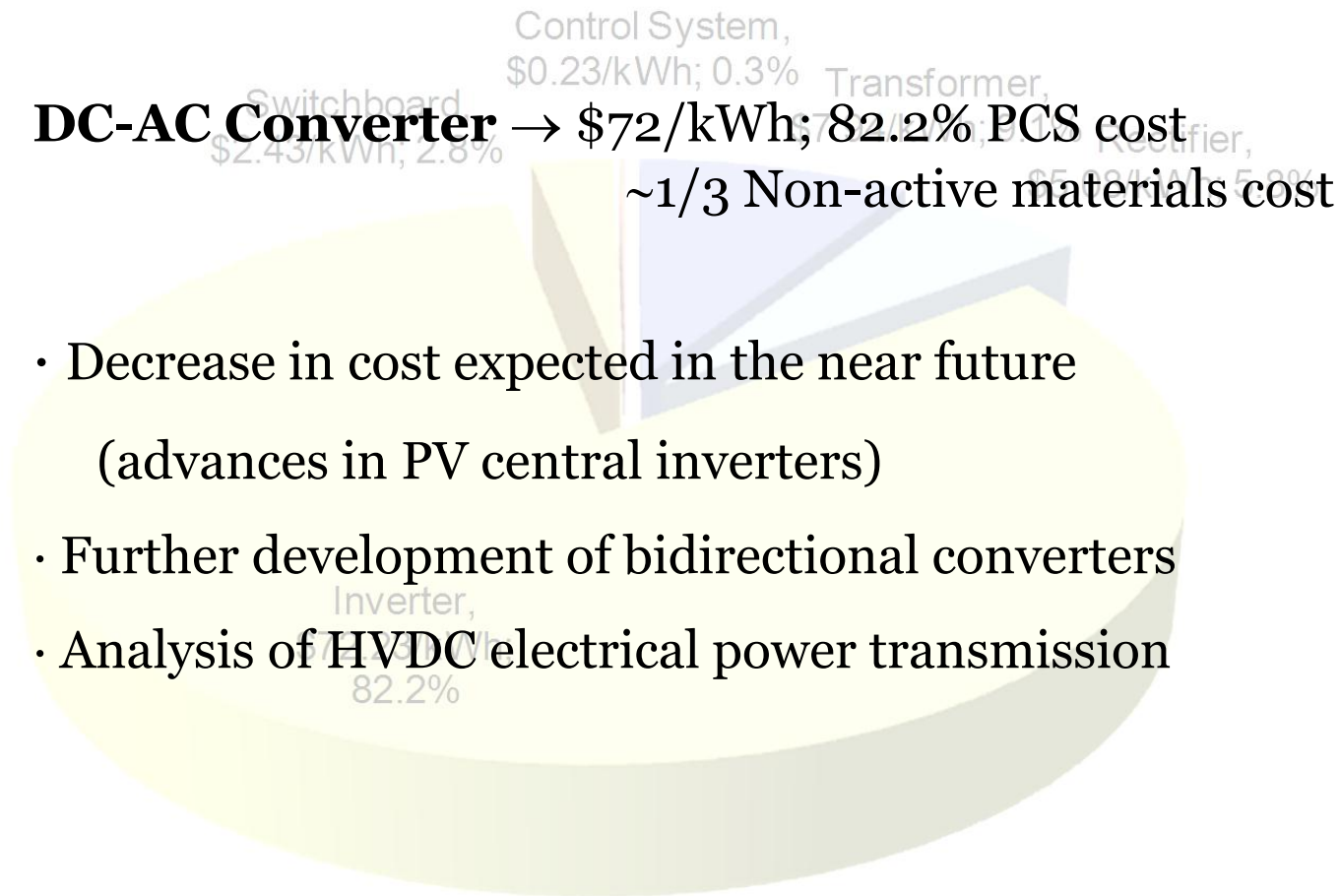


PCS Total cost \$87.88/kWh

*Critical cost:*

**DC-AC Converter** → \$72/kWh; 82.2% PCS cost  
 ~1/3 Non-active materials cost

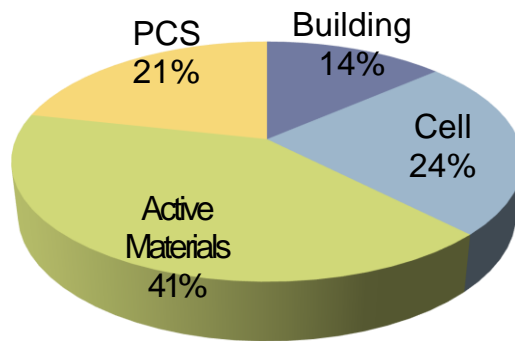
- Decrease in cost expected in the near future  
 (advances in PV central inverters)
- Further development of bidirectional converters
- Analysis of HVDC electrical power transmission



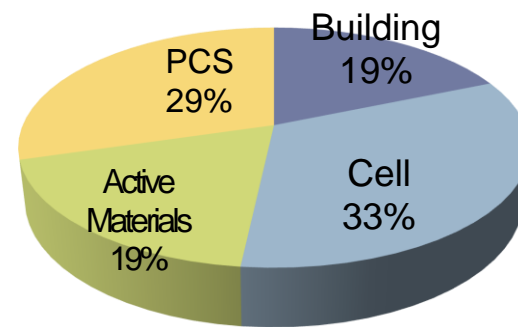
# sensitivity analysis



**LMB A, \$408.26/kWh**

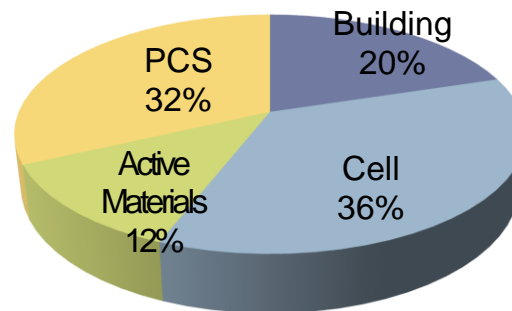


**LMB B, \$297.15/kWh**



Initial case

**LMB C, \$274.93/kWh**



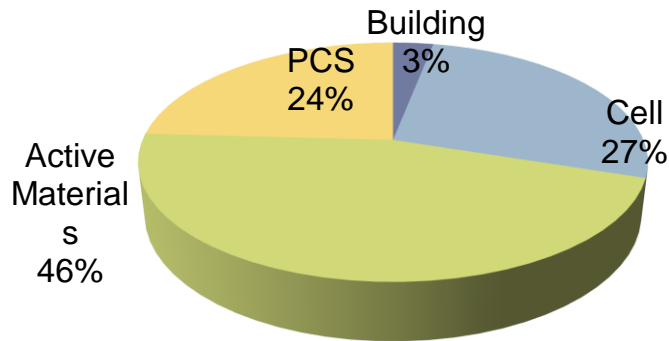


# sensitivity analysis

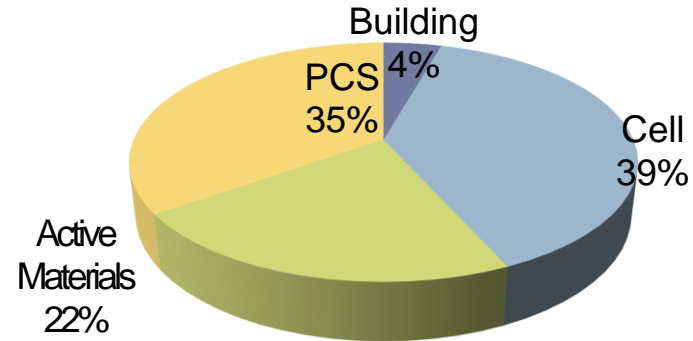


## Five Levels of Cells

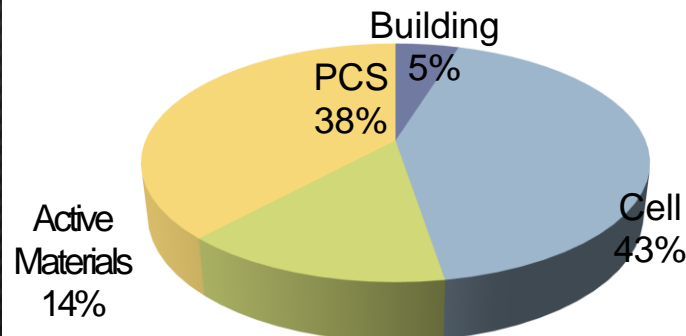
**LMB A, \$363.82/kWh**



**LMB B, \$252.71/kWh**



**LMB C, \$230.49/kWh**



# sensitivity analysis



## Five Levels of Cells

	LMB A		LMB B		LMB C	
	Base Scen	Scen One	Base Scen	Scen One	Base Scen	Scen One
<b>\$/kWh</b>	408.26	363.82	297.15	252.71	274.93	230.49
<b>Ratio</b>	0.89		0.85		0.84	
<b>% Building</b>	14%	3%	19%	4%	20%	5%
<b>% Cell</b>	24%	27%	33%	39%	36%	43%
<b>% Active Materials</b>	41%	46%	19%	22%	12%	14%
<b>% PCS</b>	21%	24%	30%	35%	32%	38%

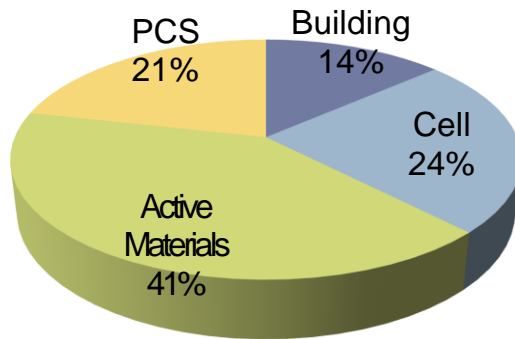
Footprint reduction: 80%  
Cost reduction: 11-16%



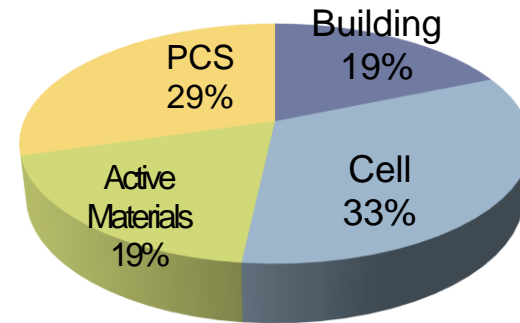
# sensitivity analysis



**LMB A, \$408.26/kWh**

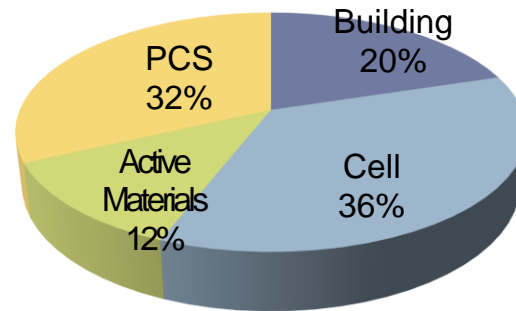


**LMB B, \$297.15/kWh**



Initial case

**LMB C, \$274.93/kWh**

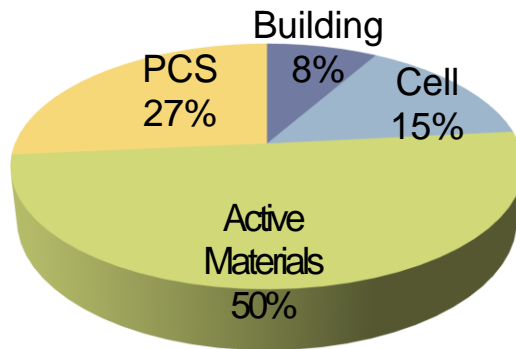


# sensitivity analysis

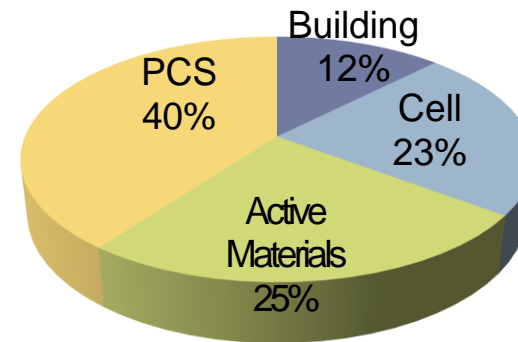


## Eight Cells per Group

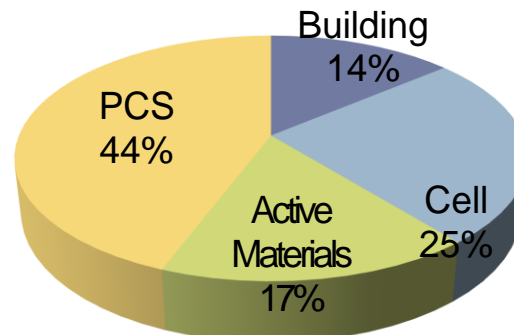
**LMB A, \$332.21/kWh**



**LMB B, \$221.1/kWh**

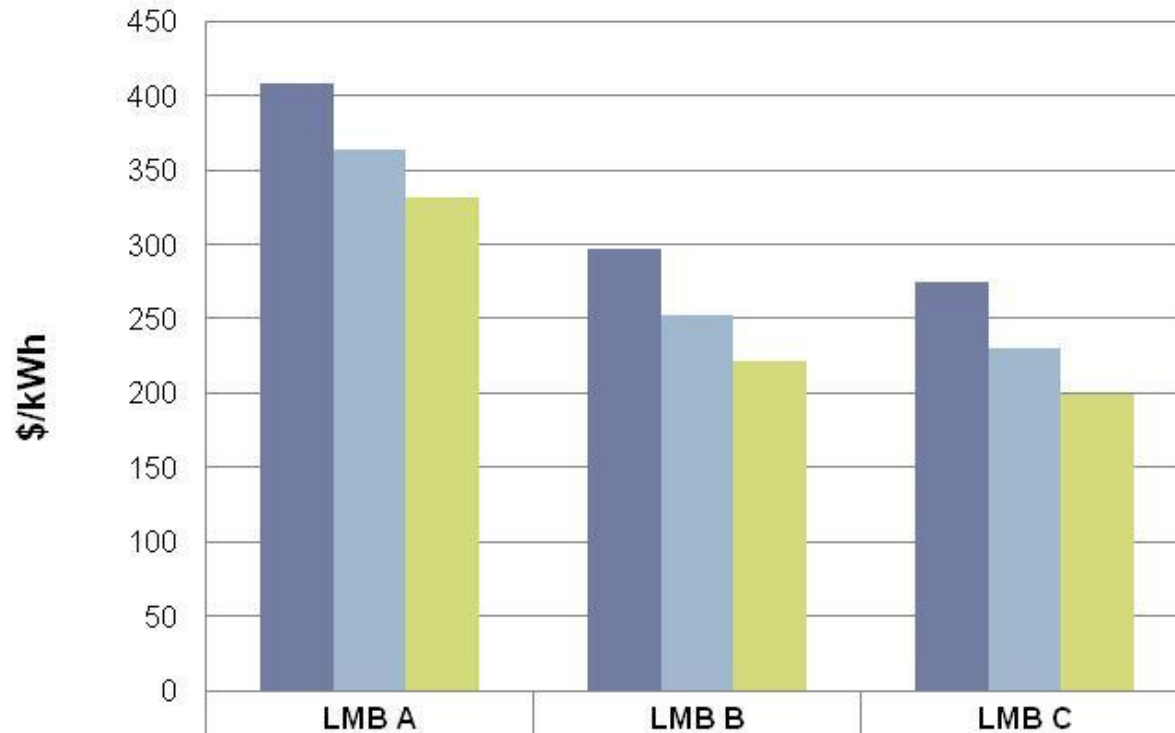


**LMB C, \$198.88/kWh**





# sensitivity analysis



	LMB A	LMB B	LMB C
■ Base Scenario	408,26	297,15	274,93
■ Scenarion One	363,82	252,71	230,49
■ Scenario Two	332,21	221,1	198,88

# conclusion



## Critical Points:

- Power Conversion System → need to reduce cost of the inverter
- Current-Efficiency relationship will influence the final cost (chemistry dependent)
- Non active materials cost as presently estimated exceed the market base cost threshold for the entire ESS
- Specific design of pot for LMB can reduce significantly the cost of ESS



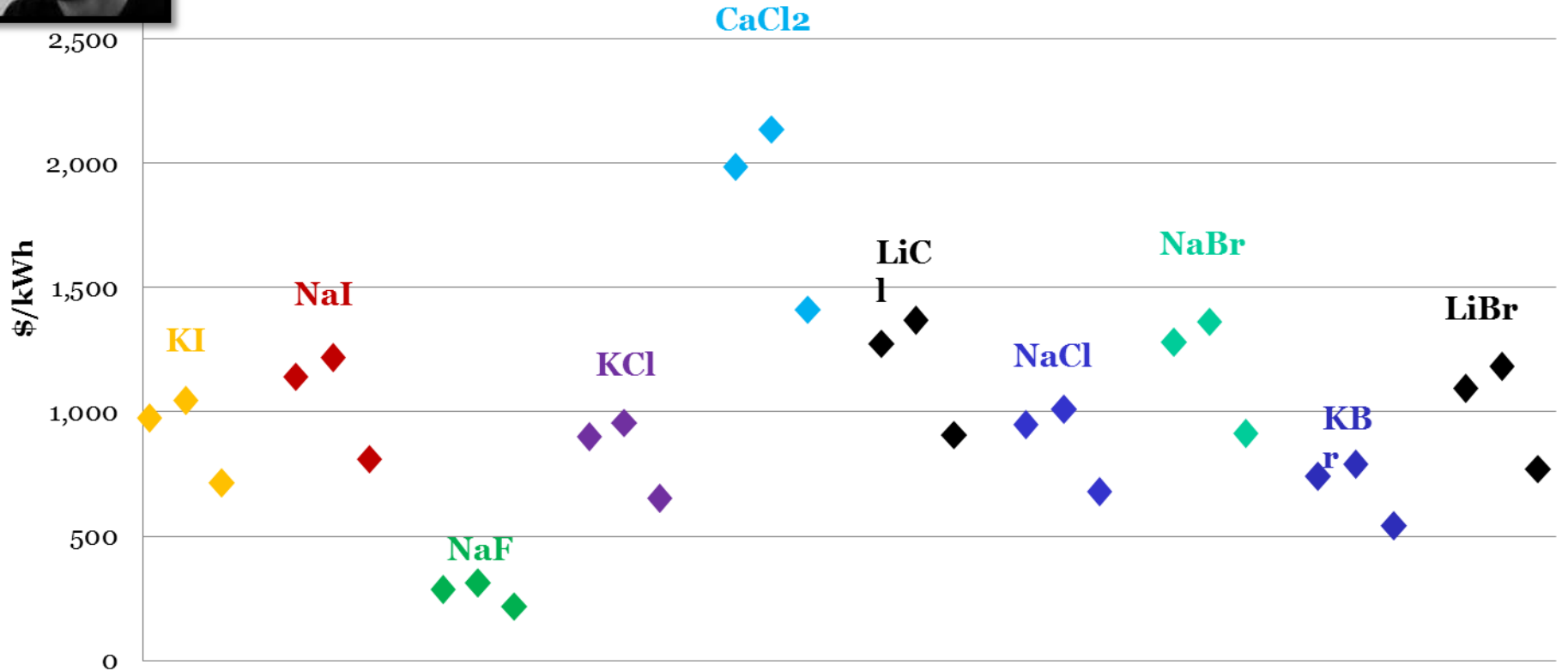
# masters thesis #4



Michael Parent

- ◉ based on most recent understanding of LMB chemistries and secondary components
- ◉ analyzed materials scarcity and cost sensitivity for LMB couples
- ◉ modeled total installed cost estimate for LMB systems based on a  $1\text{m} \times 2\text{m}$  cell size
- ◉ identified dry salt costs as important cost control target

# lab grade salt costs



salts used for testing are extremely expensive



# lab scale purification



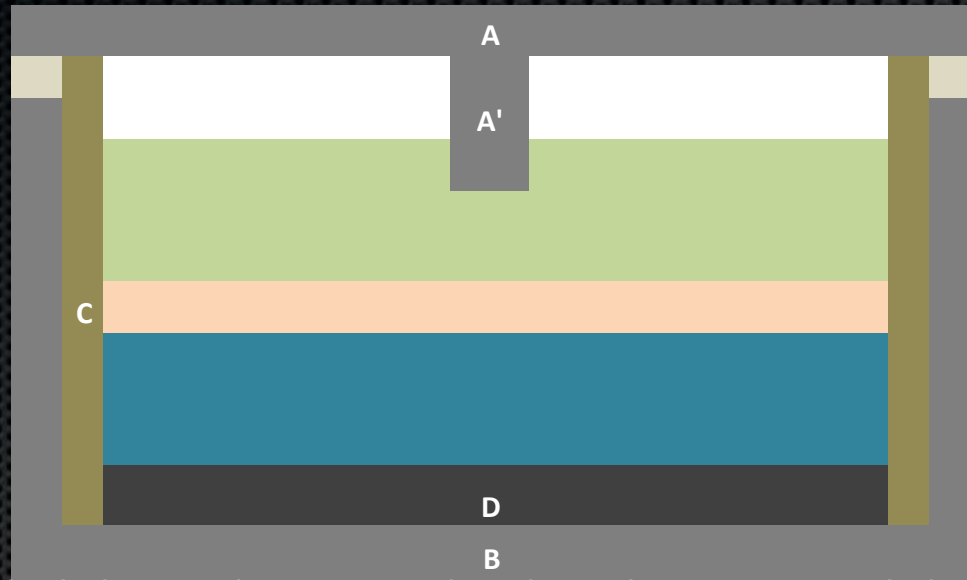
Salt	Retail (\$/kWh)	Bulk (\$/kWh)	In-House* (\$/kWh)	% Savings
NaF	17	0.35	9	47%
NaI	463	17	246	47%
NaCl	447	0.01	240	46%
NaBr	854	7	458	46%
KCl	780	0.11	419	46%
KI	555	12	296	47%
LiCl	838	10	449	46%
LiI	622	103	314	50%
LiBr	752	15	401	47%
CaCl <sub>2</sub>	1,220	0.12	656	46%
KBr	414	9	221	47%

\*Assumes 93% product yield

Energy cost taken from a Gen 3 cell at 0.5 A/cm<sup>2</sup>

# cell Enclosure

## cell enclosure cost estimate



Material	Part	Cost (\$/kg)	\$/kWh
Steel	A,A',B	0.55 [1]	6.7
Alumina	C	100.00 [2]	22.5
Graphite	D	1.50 [3]	1.7
Copper	wiring	9.75 [4]	1.3
various	misc.	NA	2.5

total: \$35/kWh

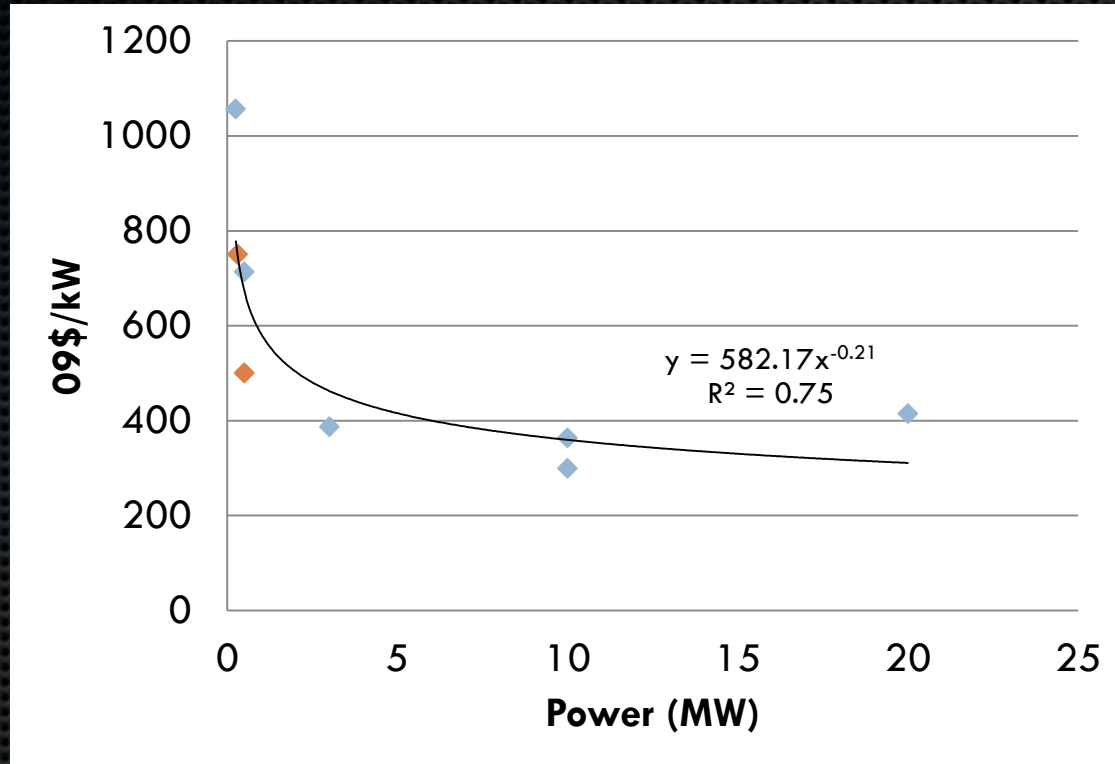


# Battery Enclosure structure cost estimate



- footprint cost of \$5,000/m<sup>2</sup>
- varies based on stacking structure
  - ➔ \$22-\$33/kWh for this model

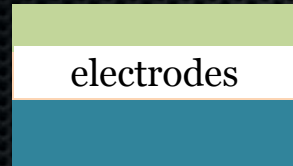
# PCS cost estimate



- higher power systems have lower unit costs (\$/kW)
- 1 MW → \$582/kW
- assume \$600/kW (\$75/kWh)



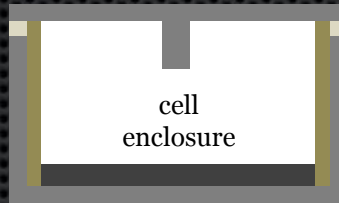
# component summary



\$34-\$486



\$17-\$1200



\$35-\$203



\$75



\$22-\$33

## results



Technology	Total system cost (\$/kWh)
Pb-Acid	750-1000 <sup>[1]</sup>
NaS	571 <sup>[2]</sup>
ZEBRA	680 <sup>[3]</sup>
Li-ion	1500-3500 <sup>[1]</sup>
LMB-Gen2	1000 <sup>[4]</sup>
LMB-Gen2	225 <sup>[4]</sup>

electrolyte  
\$817/kWh

electrolyte  
\$20/kWh





LIQUID METAL BATTERY CORPORATION

LMB C



- ◉ founded 2010
- ◉ series A from 'patient' investors
- ◉ focus on commercialization & scale-up
- ◉ validate manufacturing approach & cost-models



## high level technical stages of the company

### STAGE 1

#### Self-heated cell

- Design, build, and operate self-heated cell
- Develop key manufacturing processes



### STAGE 2

#### Stack (demonstration unit)

- Stack of cells
- System performance testing
- Deployable demonstration unit



### STAGE 3

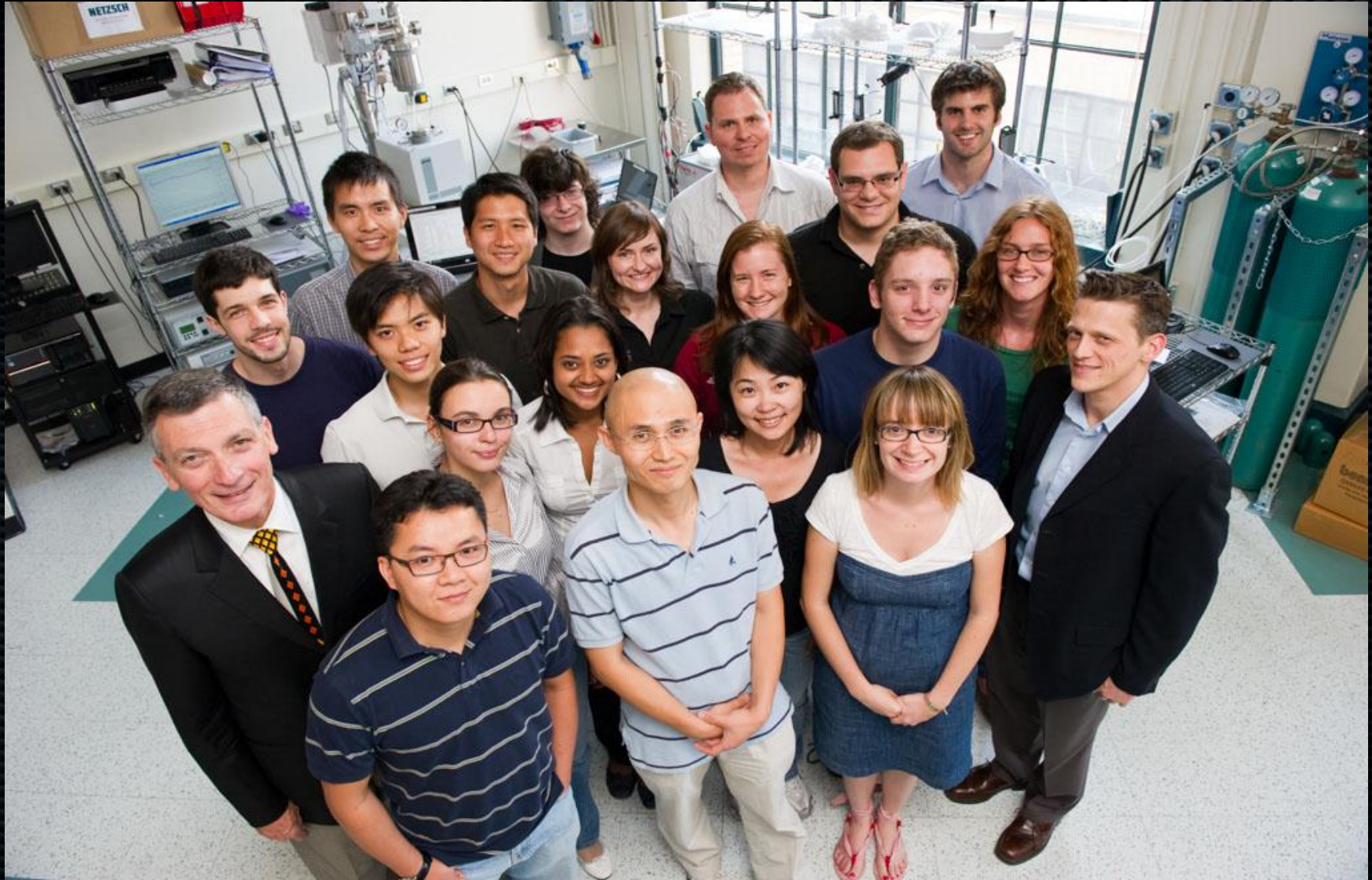
#### High volume manufacturing

- Increase production capability
- Sale to commercial buyers

End of Stage 1 Goal (*24 months*)

→ Design, construct, and operate a self-heated cell

# Liquid Metal Battery team





# sponsors

